

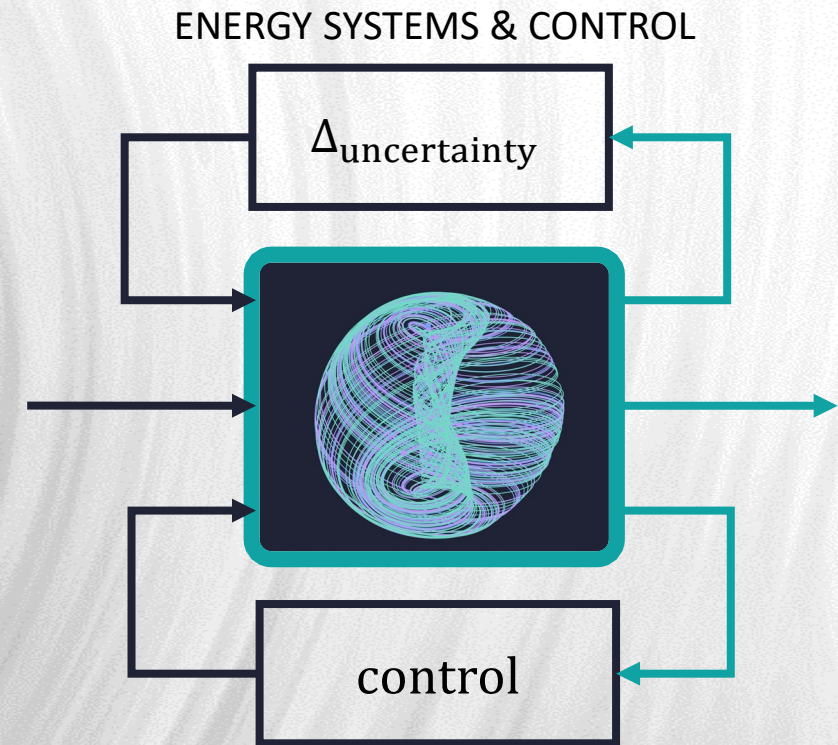
# Discussion on re-attachment times

Update on control-oriented modelling

Eurofusion

11-03-2025

**Matthijs van Berkel**, Jorn Veenendaal, Menno Lauret, Gijs Derks, Thomas Bosman, Bob Kool, Stijn Kobussen, Stefan Dasbach, Sven Wiesen, Max Winkel, Loes Jansen, JJ Palacios Roman, and the Energy Systems & Control group



# Summary of this presentation

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- Why time dependent excitations/perturbations are the same as frequency domain
  - Why multi-sines are generally better than step-responses!
- Proper re-attachment (times) analysis based on control oriented “digital twin”
- Necessity of proper impurity observer
  - Overseeding is consistently wasting significant amount of discharges
- Challenges for validation and working on the next steps?

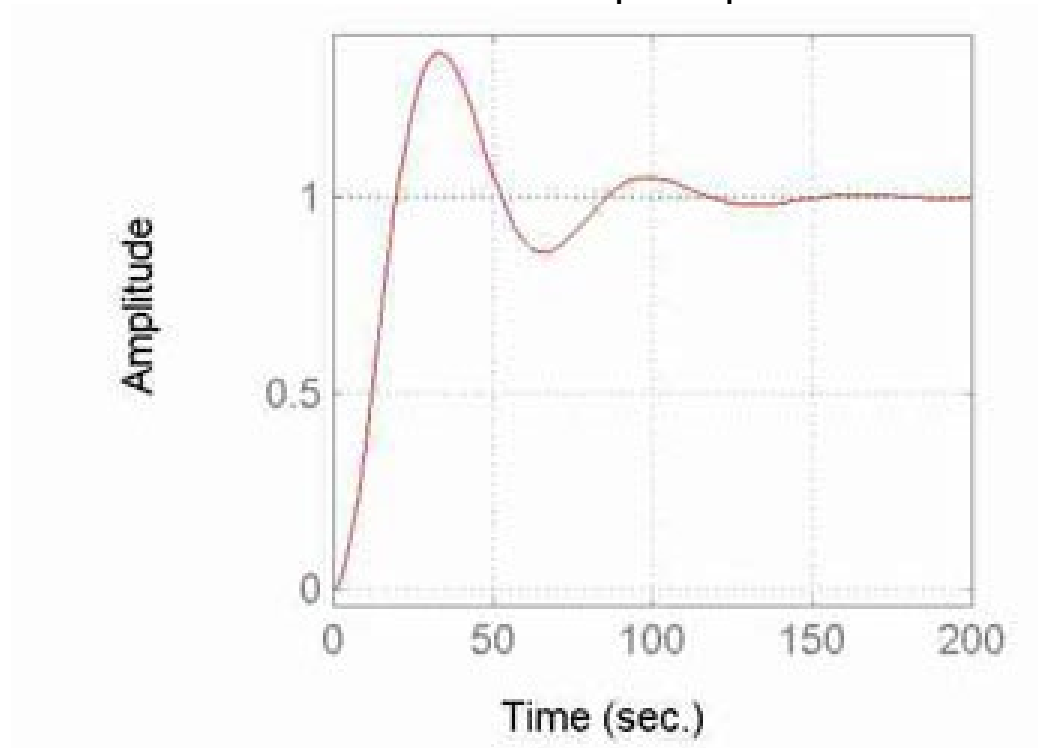


**System identification  
time (step) vs. frequency (bode)**

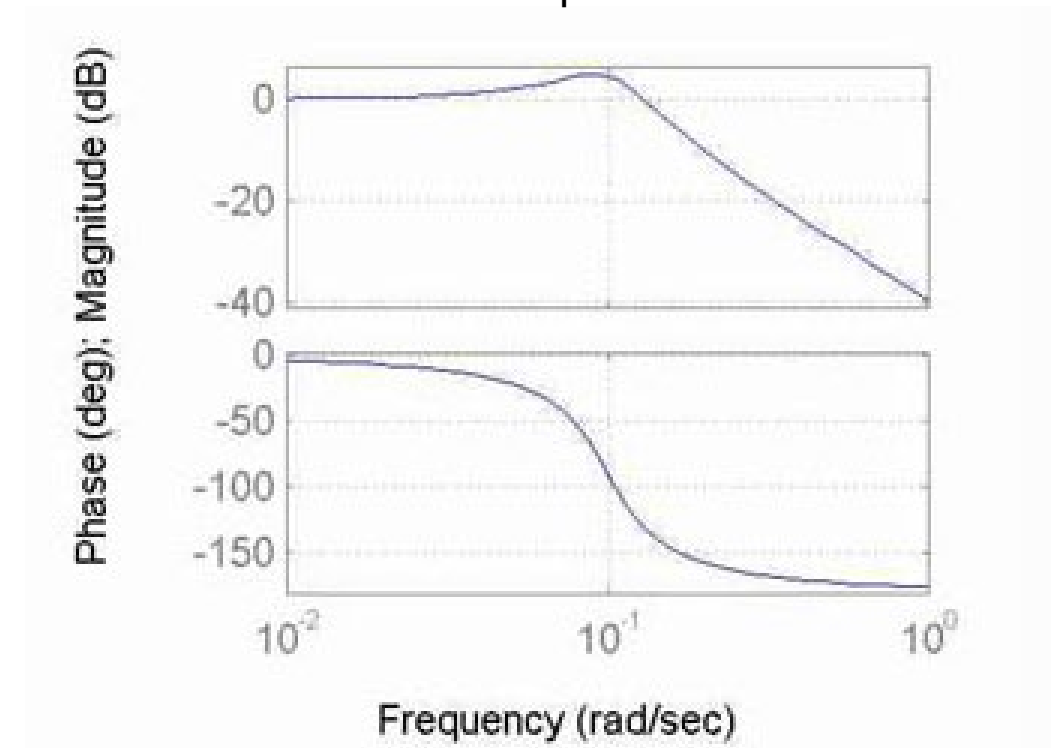
## Step responses and multi-sines identify the same (but differently)

Transient Response is the same thing as "step response"

Frequency Response is typically shown using a "Bode plot"



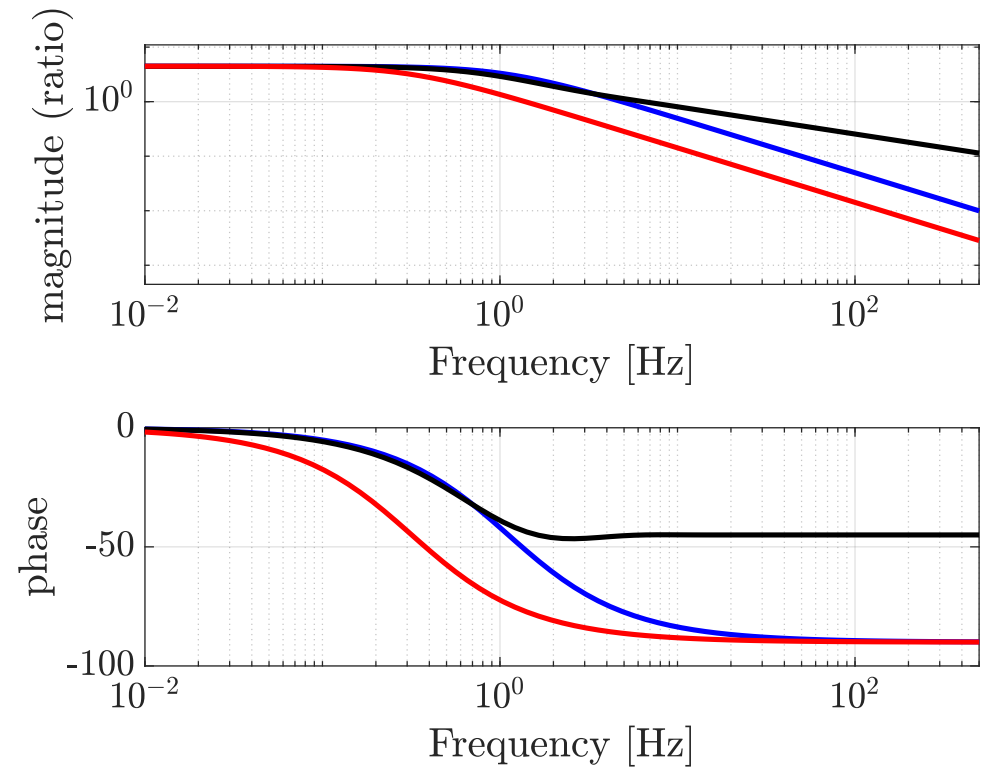
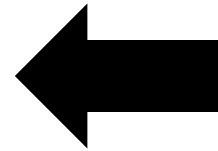
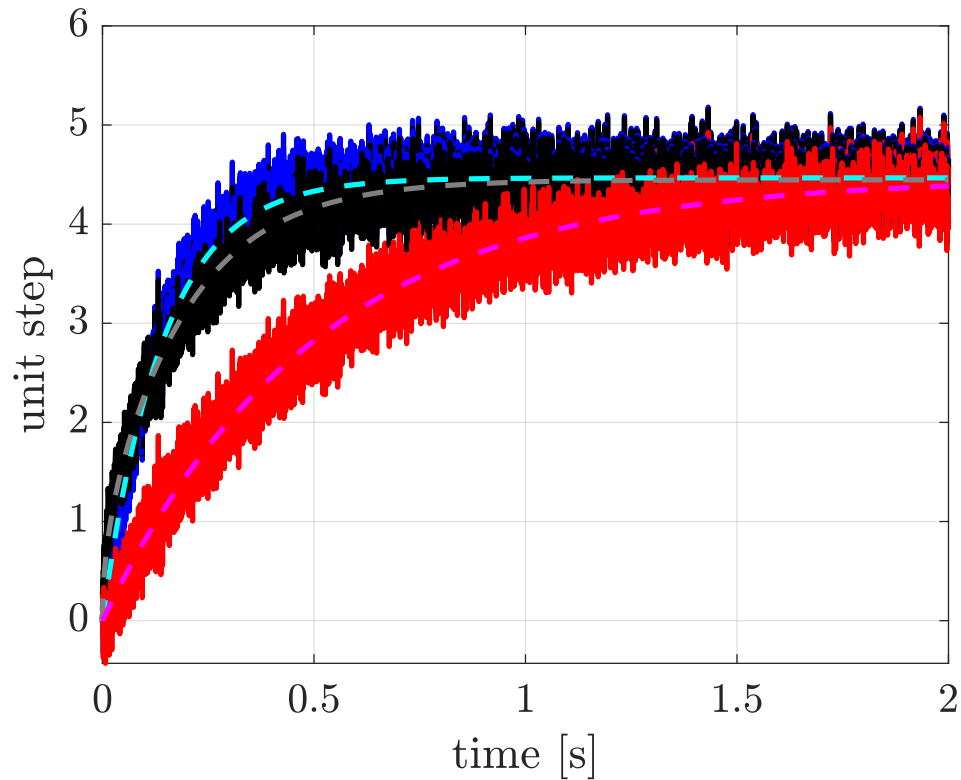
**def**  
**==**



- You make an abrupt change to the INPUT and watch the response of the OUTPUT over TIME.

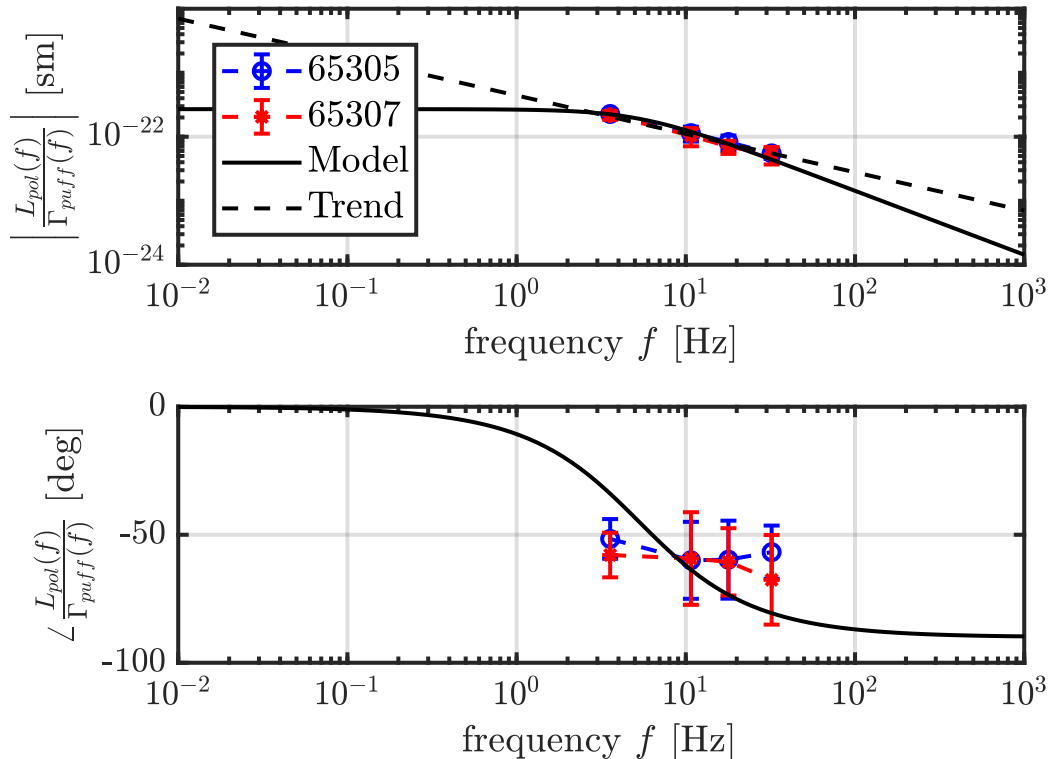
- You use a sinusoidally-varying INPUT signal at some particular frequency.
- You determine the GAIN, PHASE which is the ratio of OUTPUT/INPUT sine waves<sup>4</sup>

# Step responses more difficult to distinguish than FRF

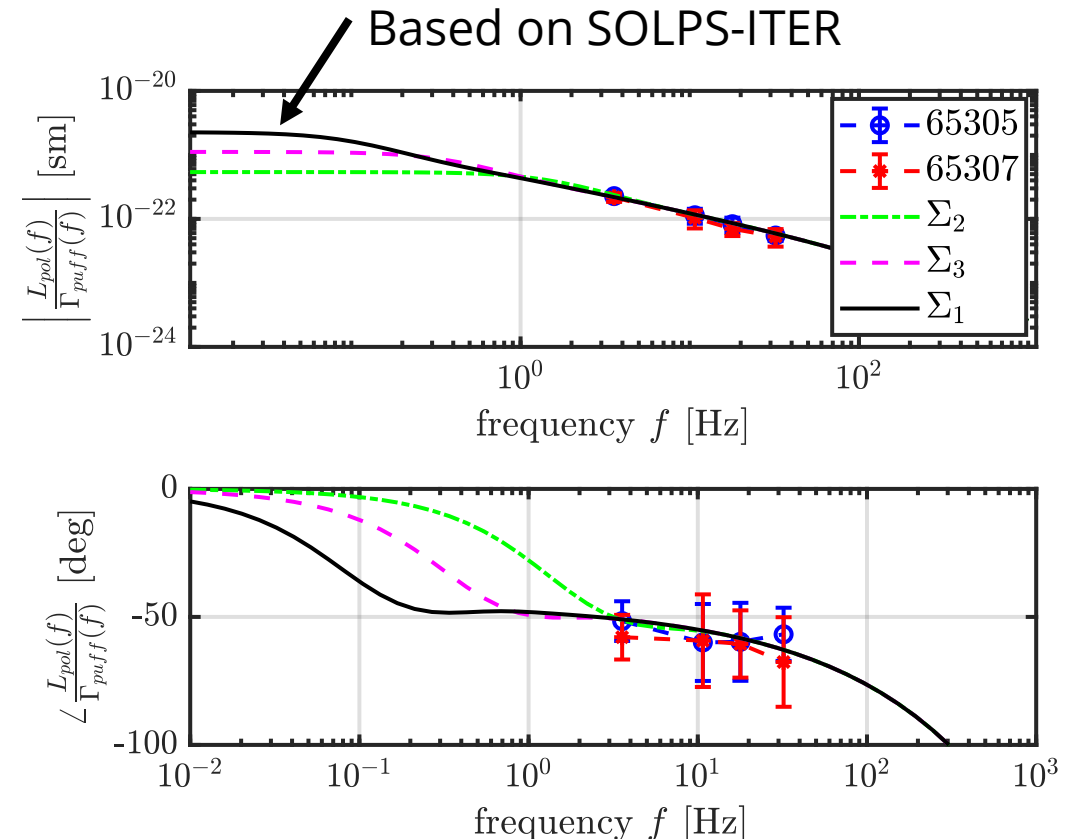




# Two simple dynamic models: fitted to data

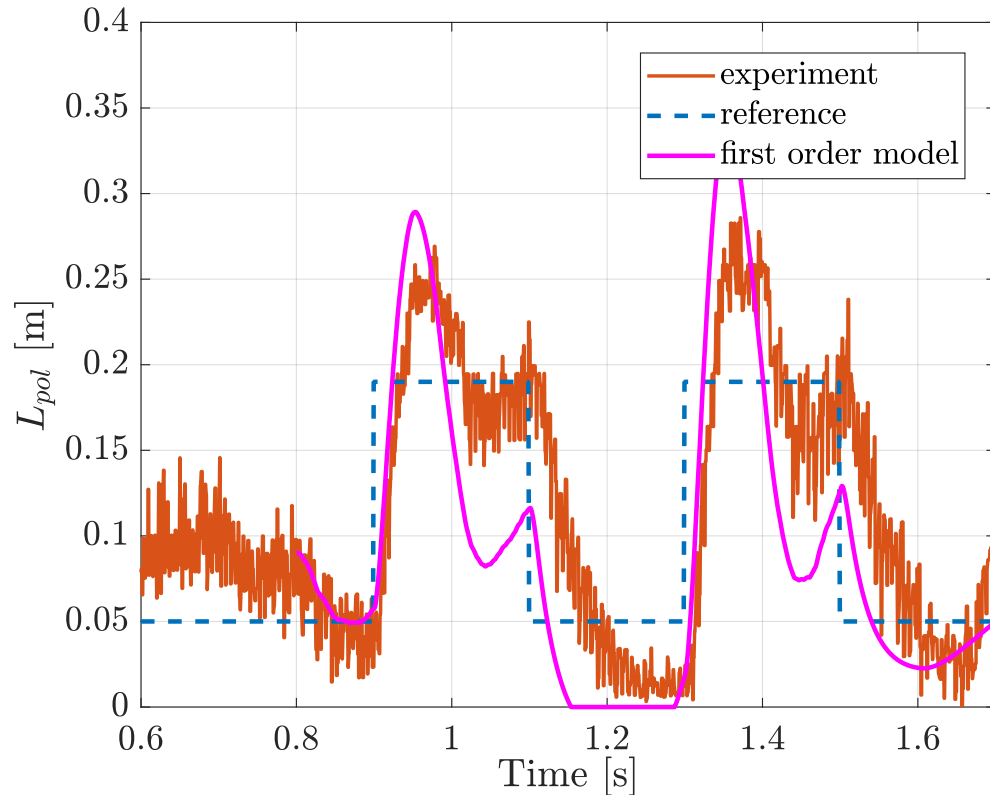


first order model (inventory)

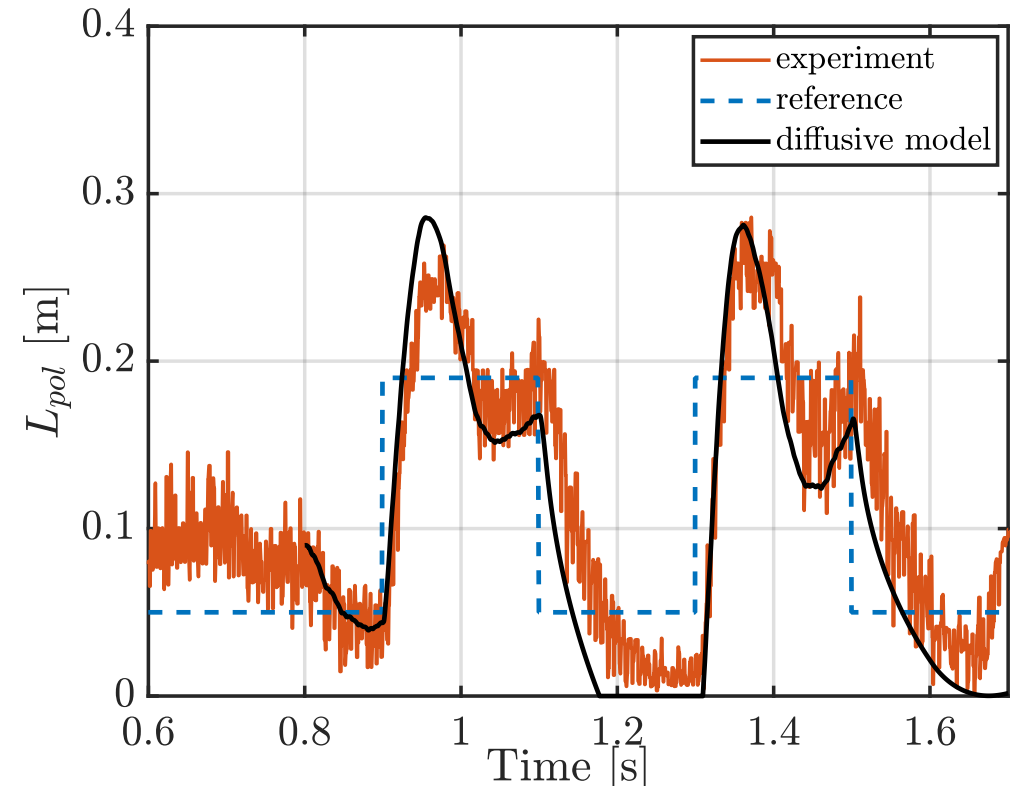


diffusive

# Improvement of dynamical models



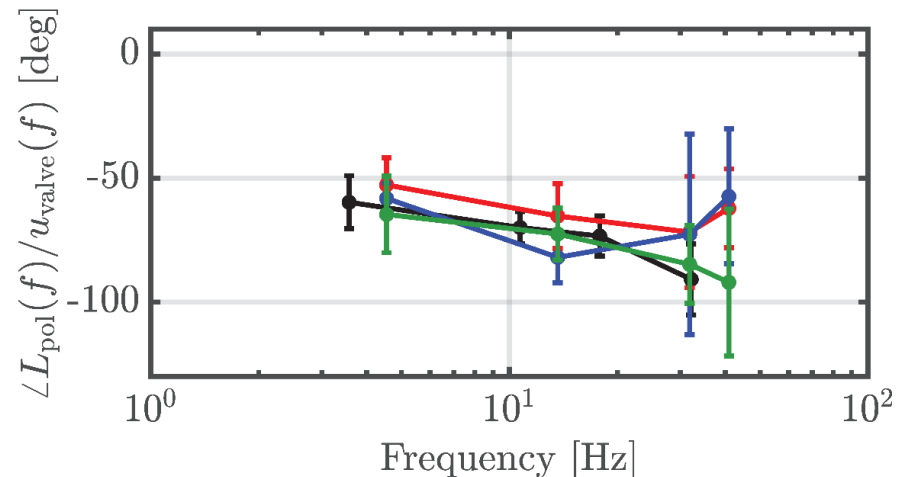
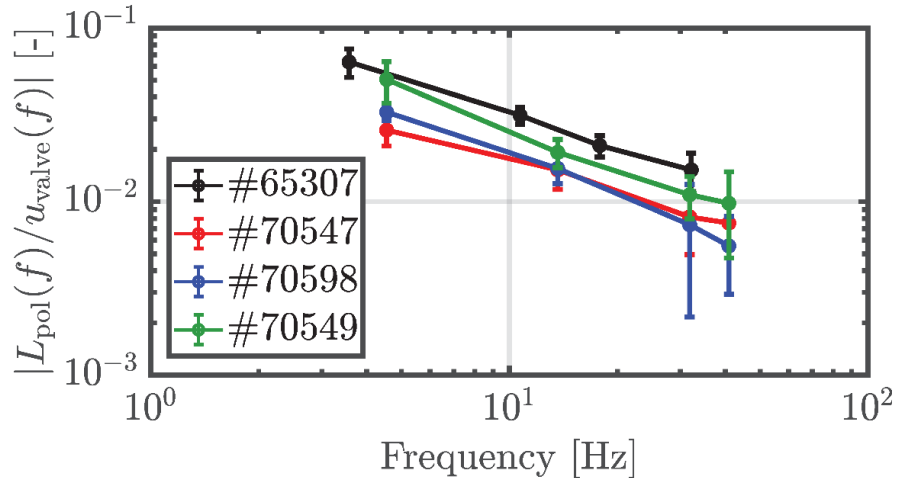
first order model (inventory)



fractional (transport)

# Non-linearity analysis (closed-loop system identification)

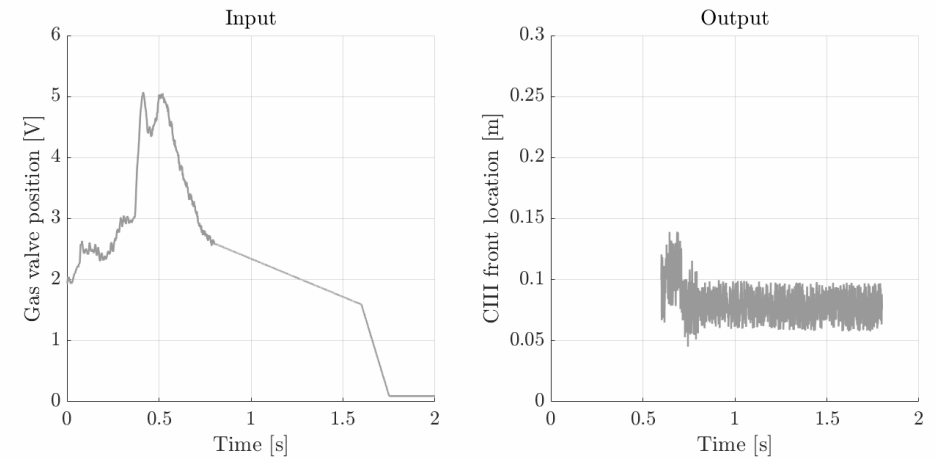
$L_{\text{pol}} = 0.09 \text{ m}$ ,  $L_{\text{pol}} = 0.17 \text{ m}$   
 $L_{\text{pol}} = 0.23 \text{ m}$ ,  $L_{\text{pol}} \approx 0.12 \text{ m (ol)}$



- Dynamics insensitive to C-III front position
- Single/linear controller sufficient within one scenario
- Same conclusion for elmy H-mode #65309, #70686, #70688, #70689
- Similar for nitrogen seeding experiments, but faster phase decay over frequency
- Weak dynamic dependence over different scenario's



# Why we use multisines instead of step responses

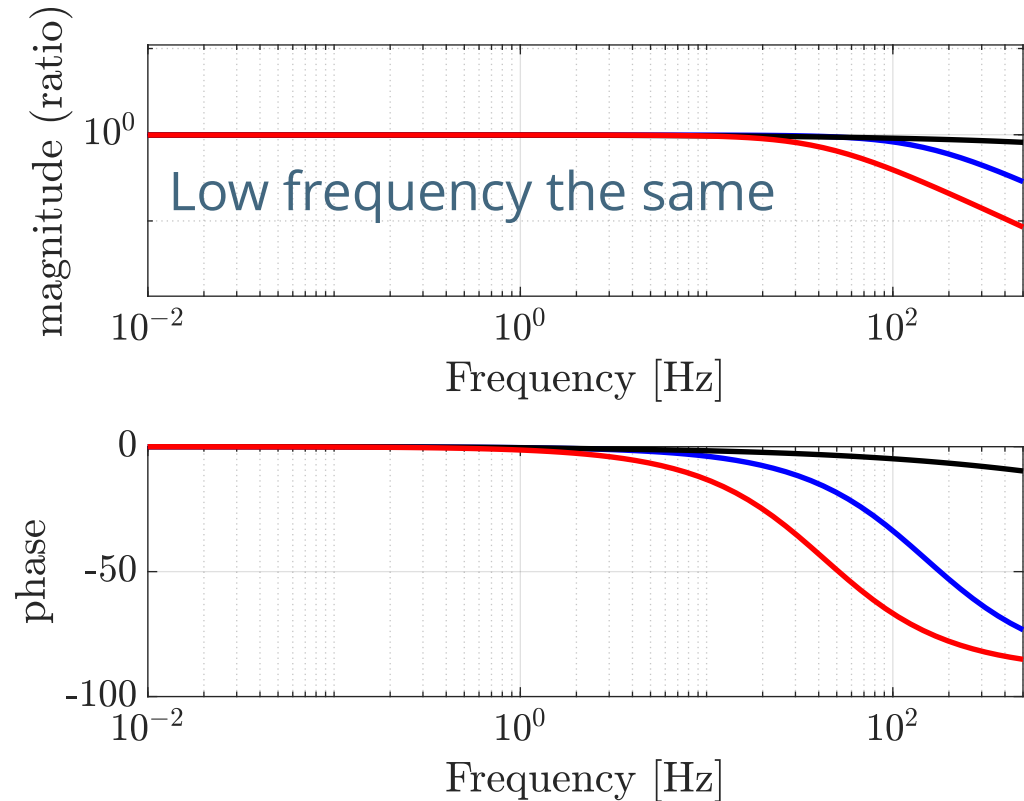
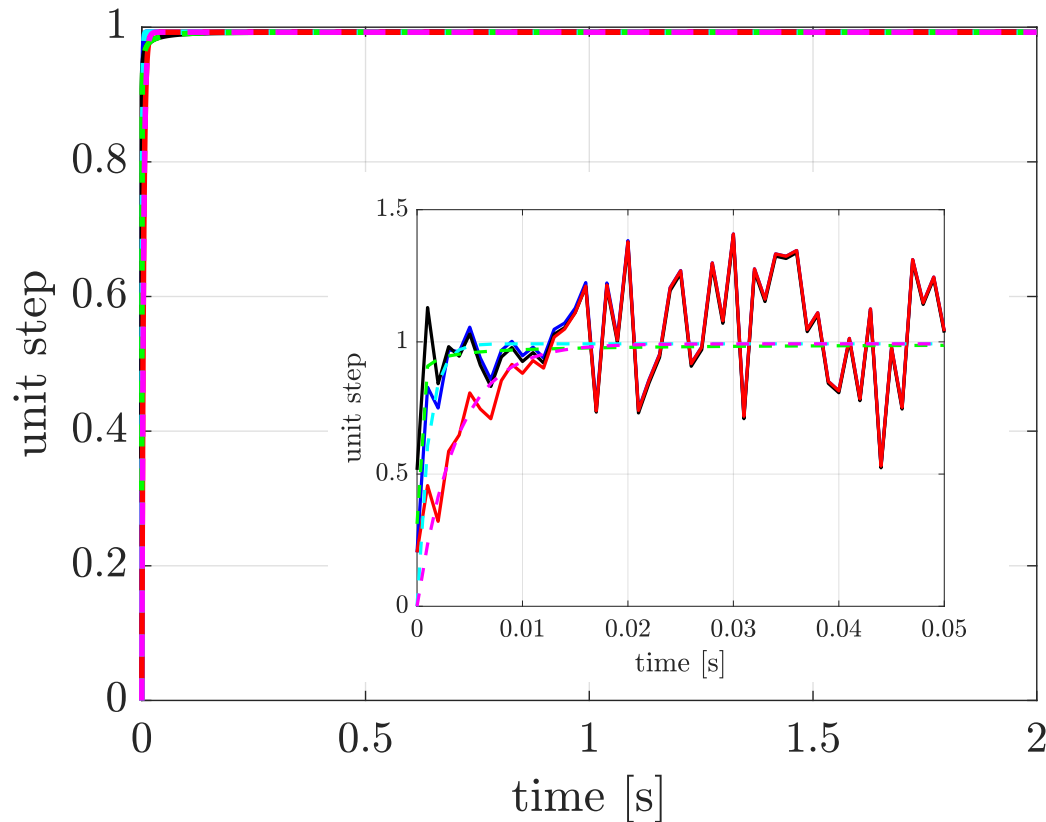


- No model free interpretation of step responses
- Exhaust is not described by a time-constant but an intermix of time-scales (follows from FRFs)
- No method to distinguish between linear and non-linear response
- Questionable convergence to equilibrium: a necessity for step responses (step down, e.g. gas cut)

Advantages multi-sines (incomplete list)

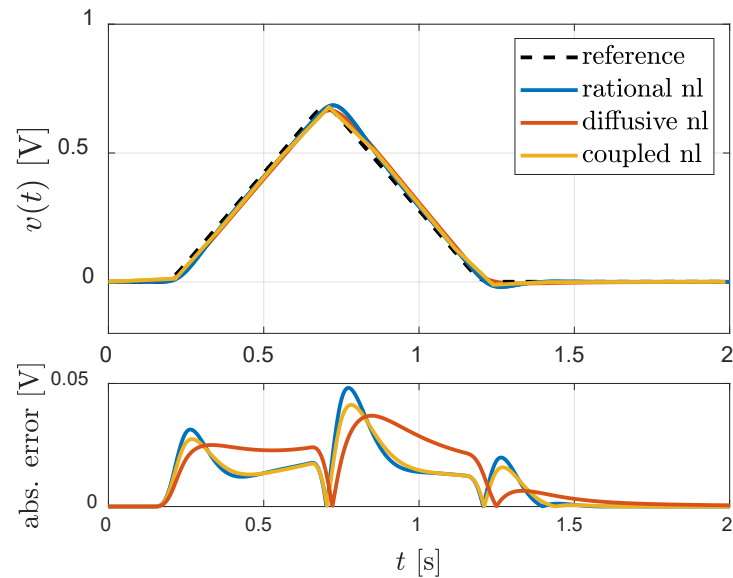
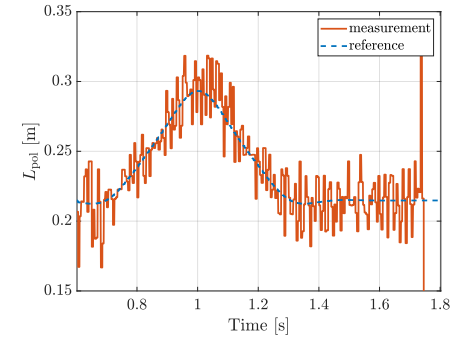
- Non-linearity tested and described over operating points
- High SNR due to averaging over periods
- Drifts/trends can be removed response does not need to go from equilibrium to equilibrium
- Model free (not fitting methods)

# Closed-loop tracking control (low frequency irrelevant)



Slow dynamics (first order approximations) suppressed by control and no longer visible/relevant in controlled scenarios

# Closed-loop: Controller stability and performance is determined by the “high frequency” dynamics

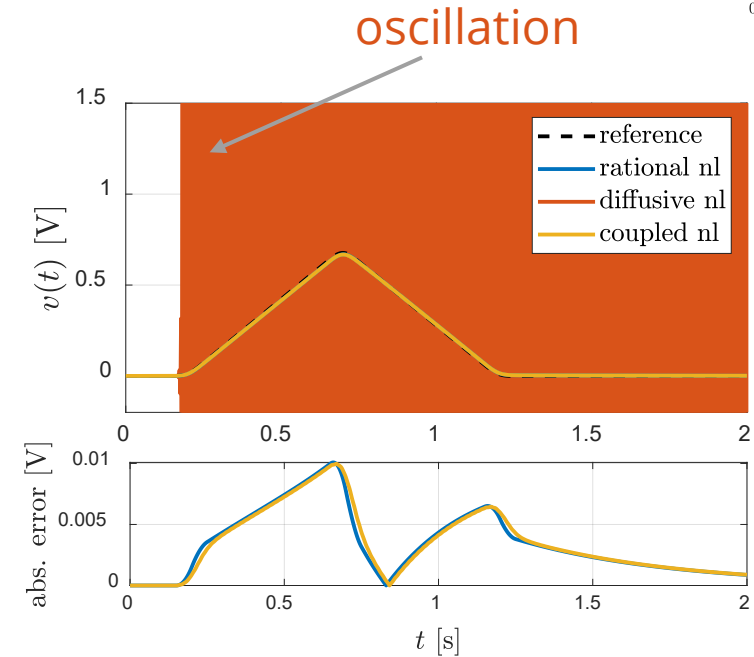


Low-performance (PI) controller

improve control



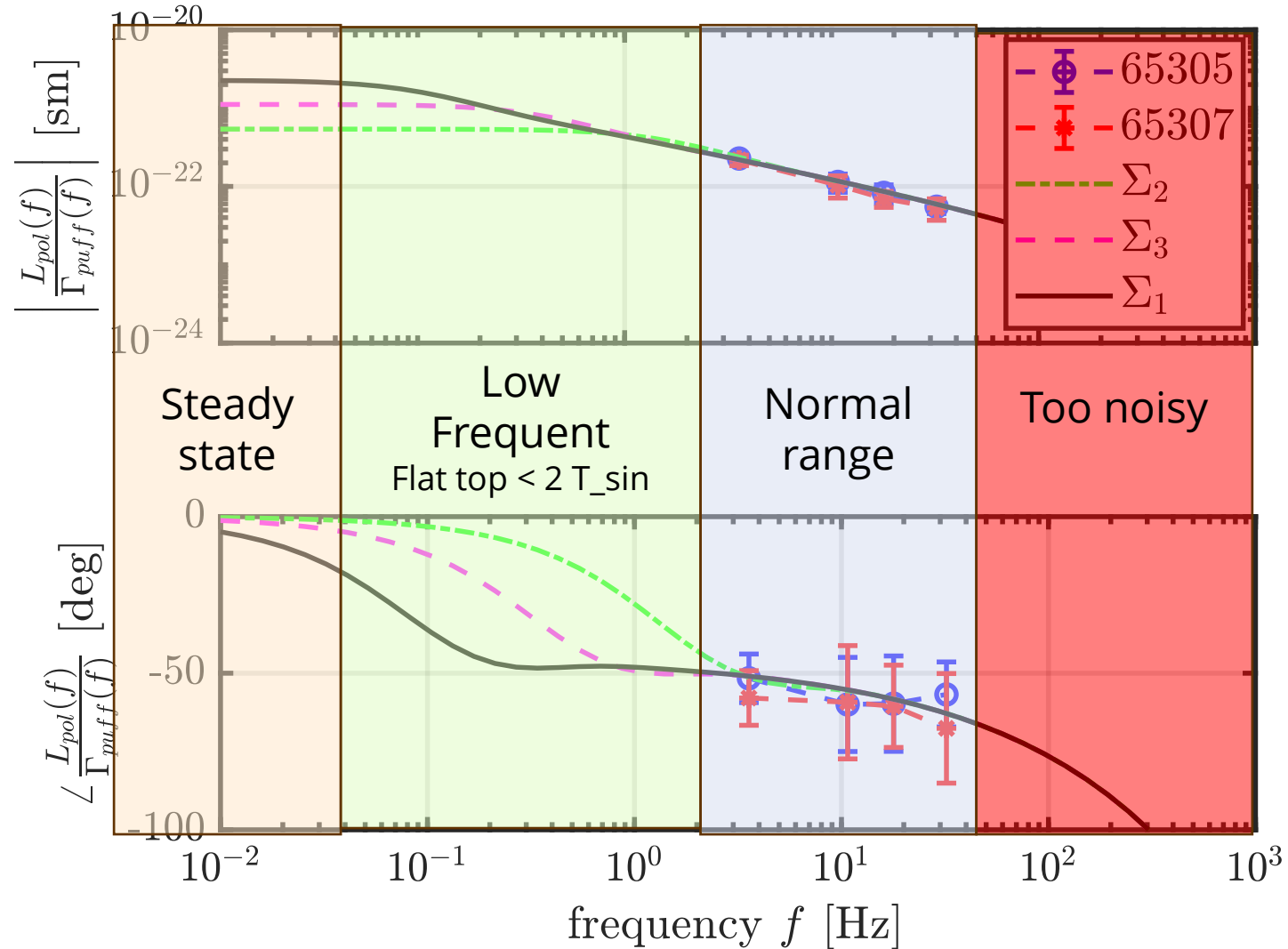
increase gain  
 $P \times 10$



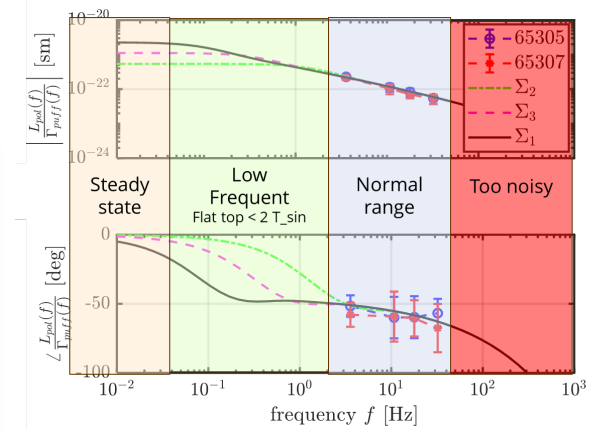
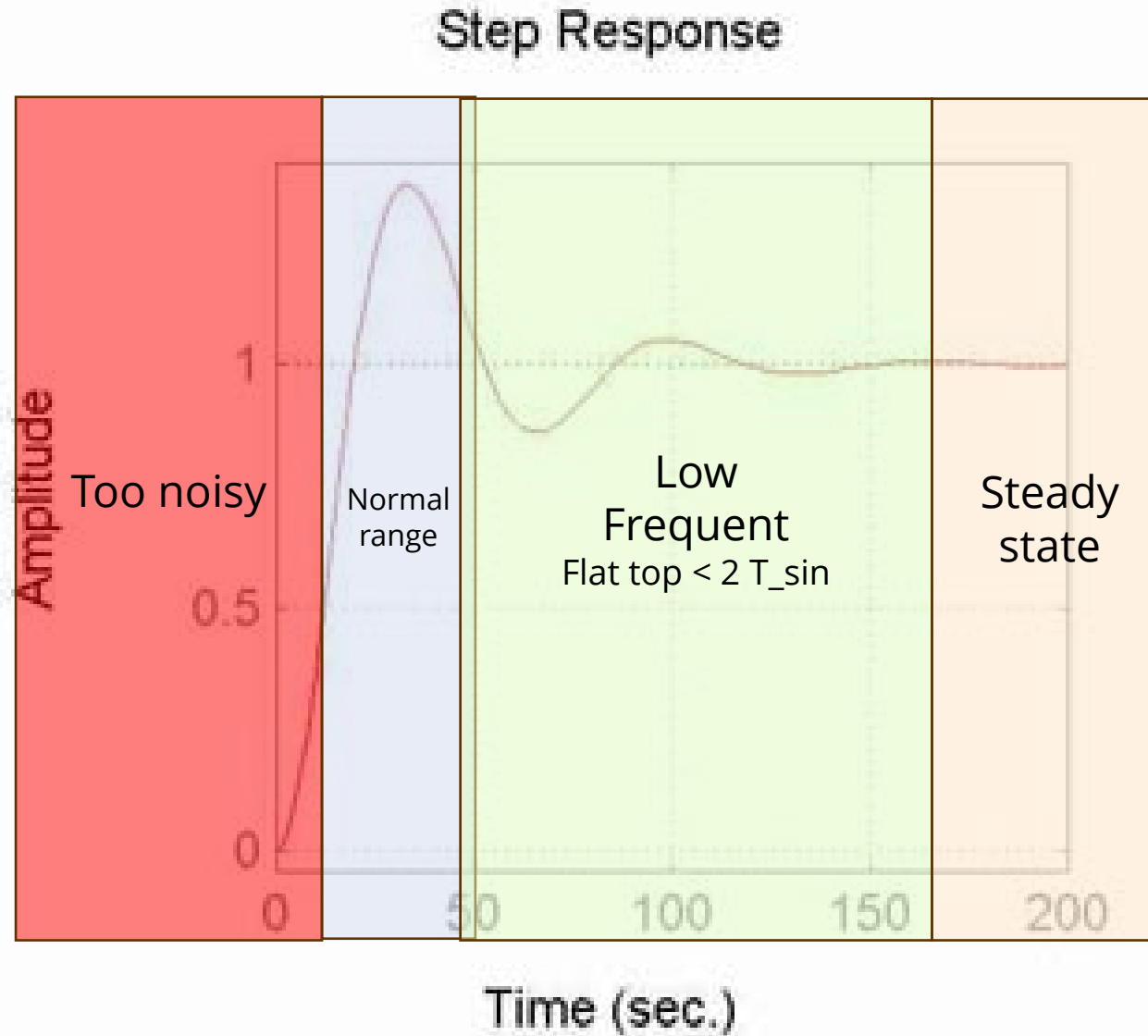
High-performance (PI) controller

- Disturbance rejection low-frequency can matter
- Extrapolation multiple timescales need to be distinguished as they are generally associated with different plasma processes

# Not all ranges are easy to measure



# Not all ranges are easy to measure



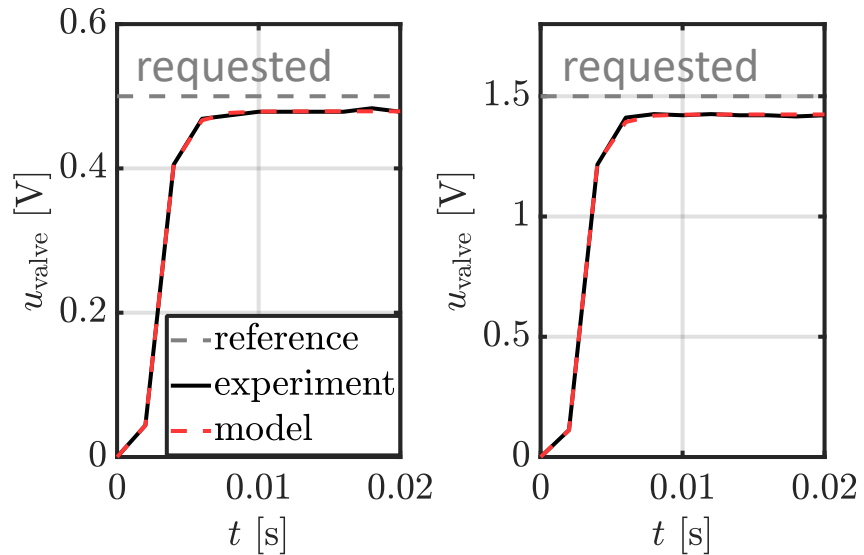


**Integration into a  
transport model**

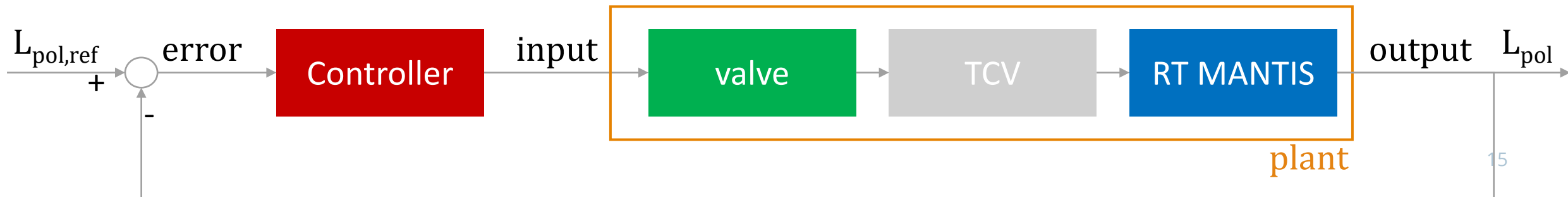
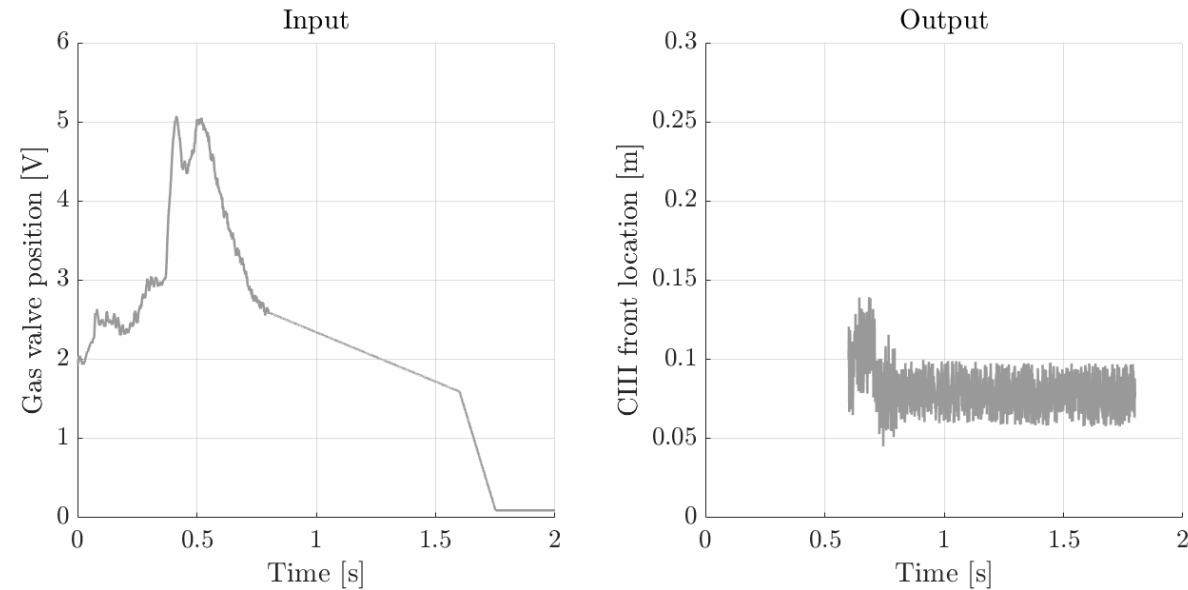


# Systematic controller design

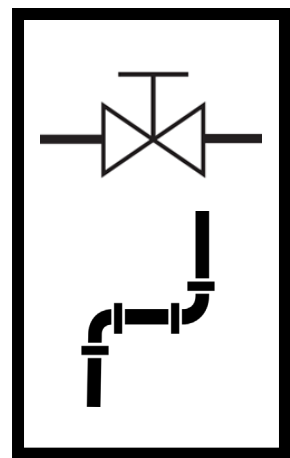
- First-order + dead time model



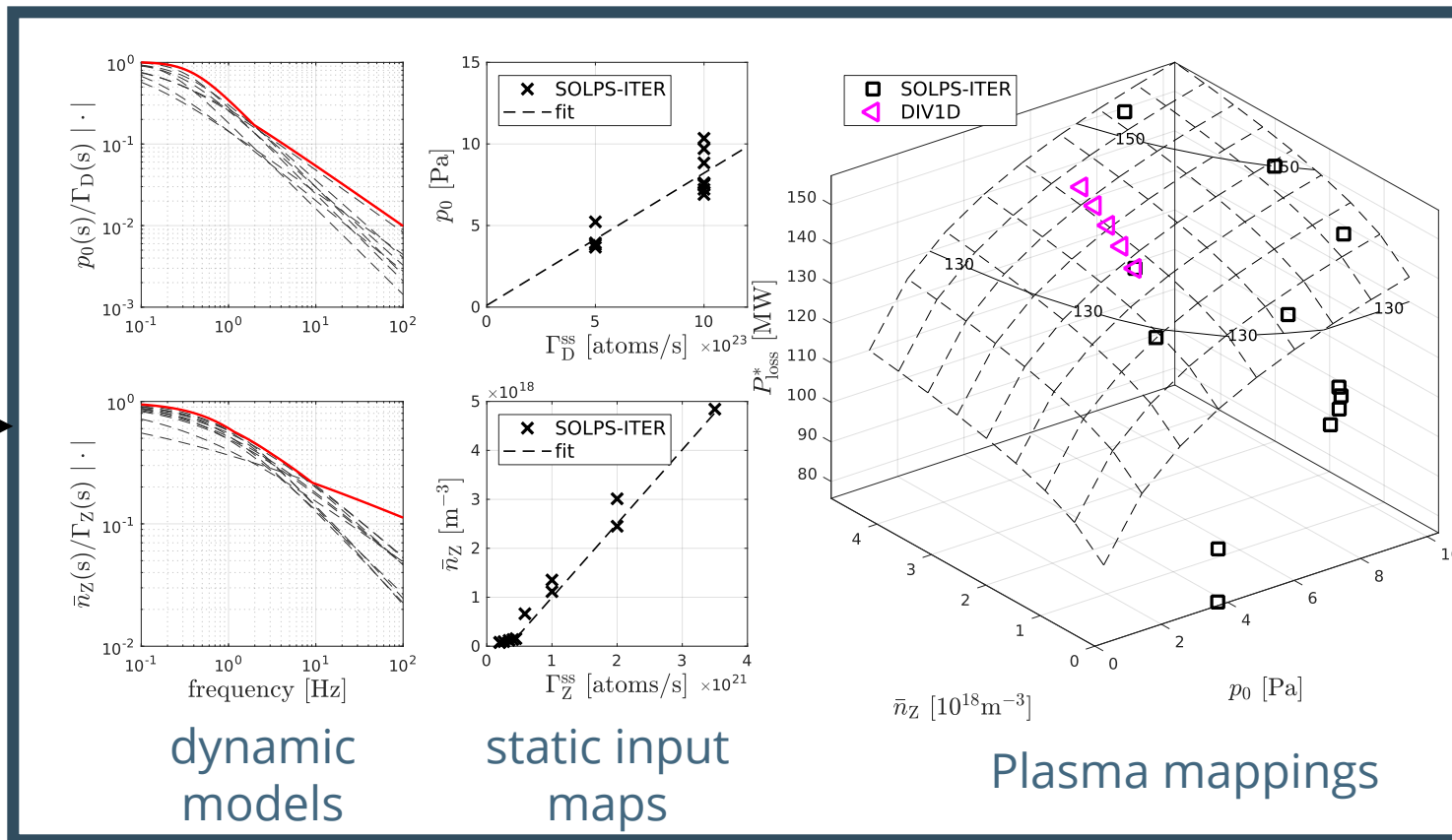
- FRF data from system identification



# Framework: ITPA DivSOL 2023 / Mosaic workshop 2023



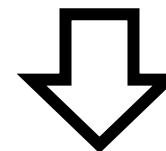
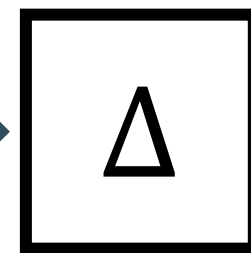
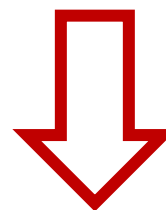
valves &  
piping  
dynamics



divertor plasma

core disturbances

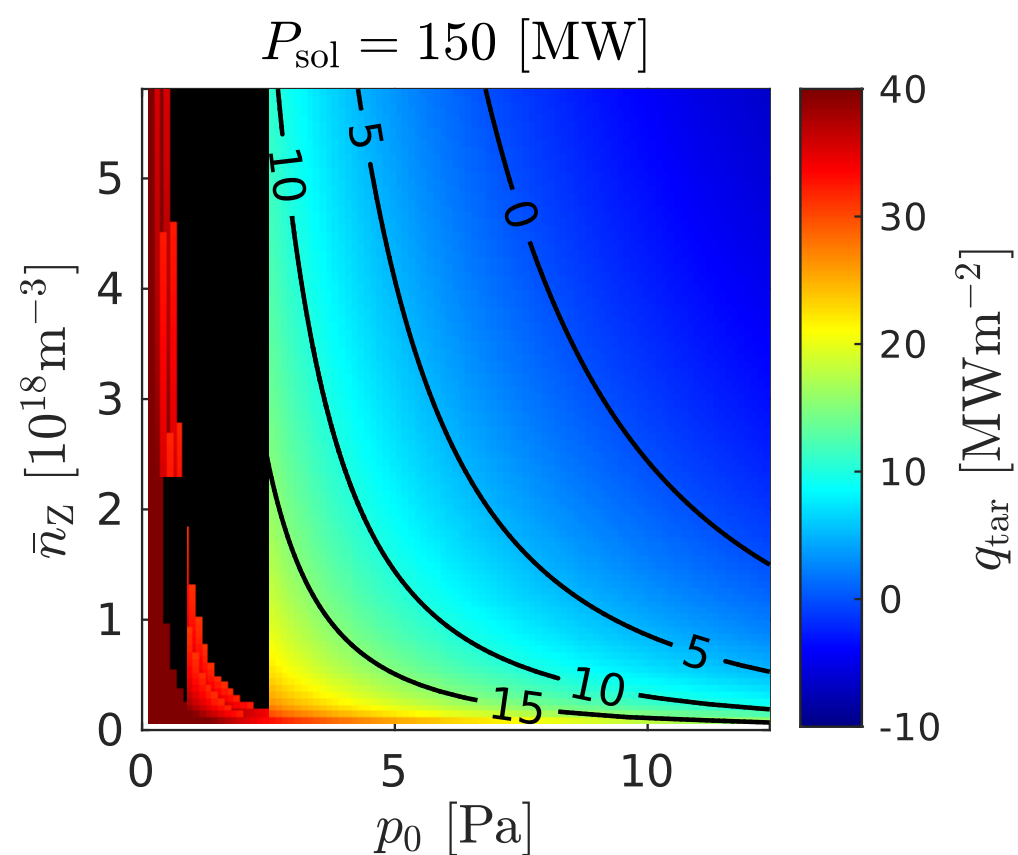
$\updownarrow P_{sol}$



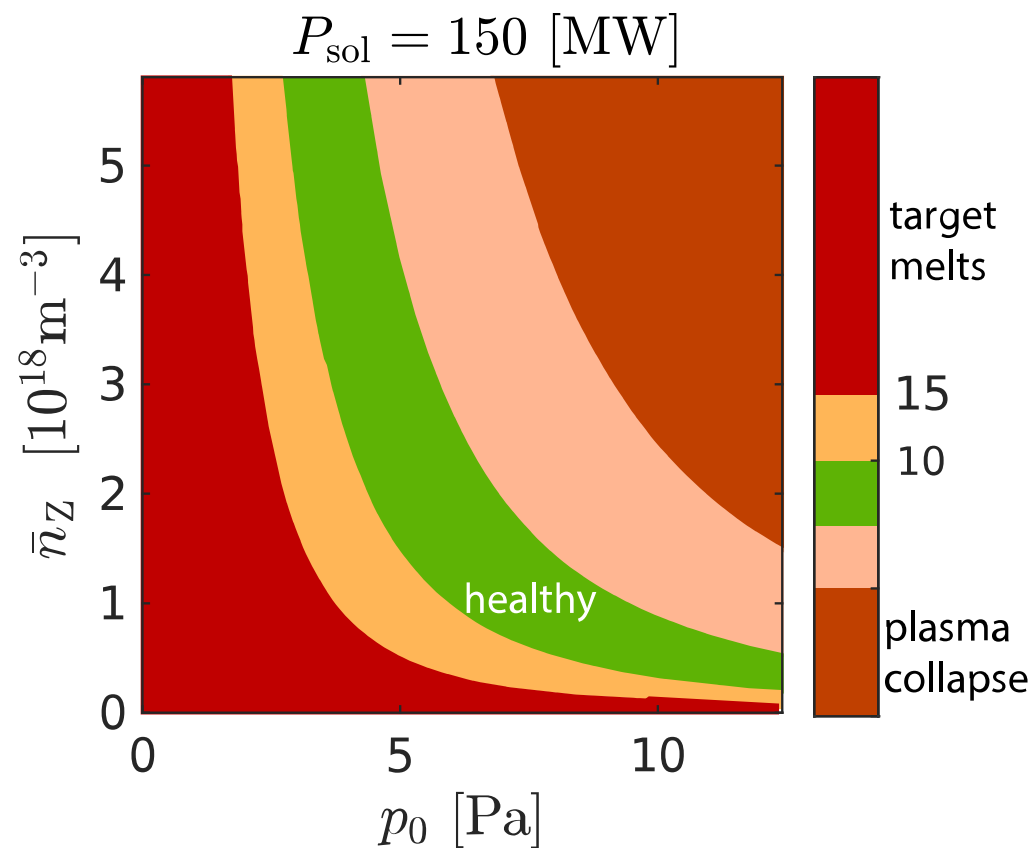
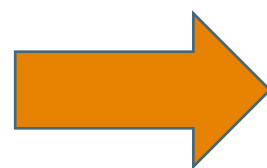
$\updownarrow q_{target}$

target conditions

# Framework: ITPA DivSOL 2023 / Mosaic workshop 2023 (cont'd)

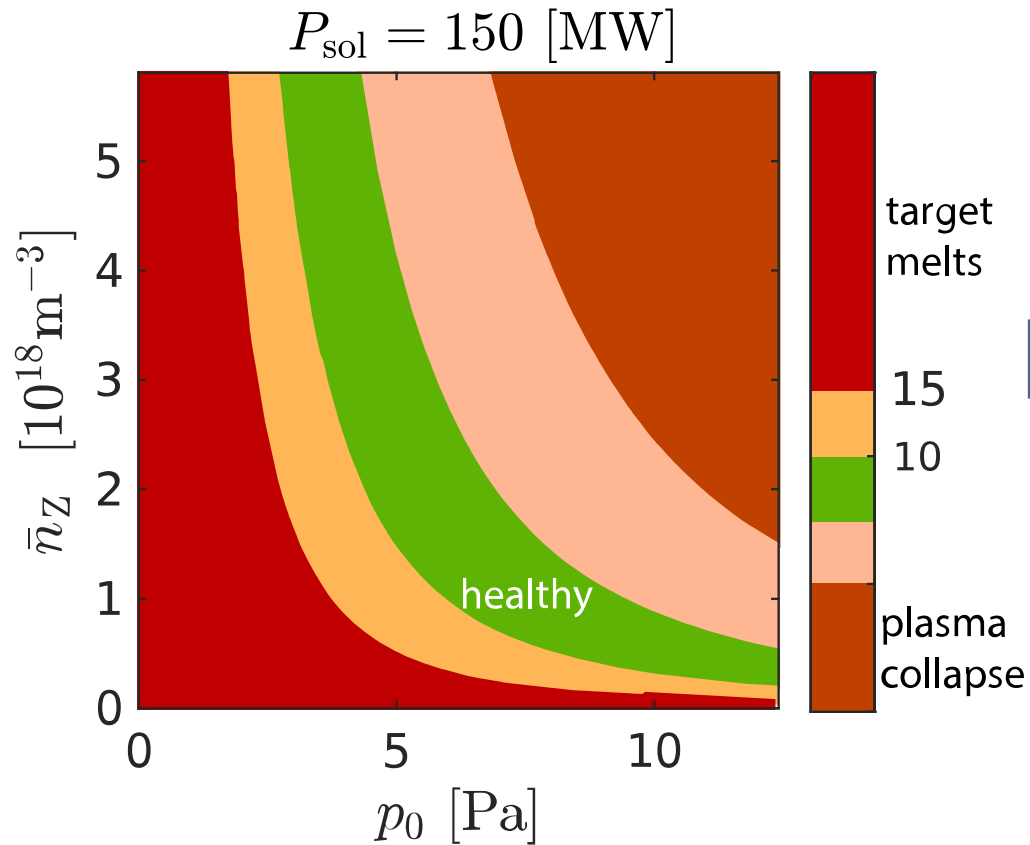


state map (simplified)

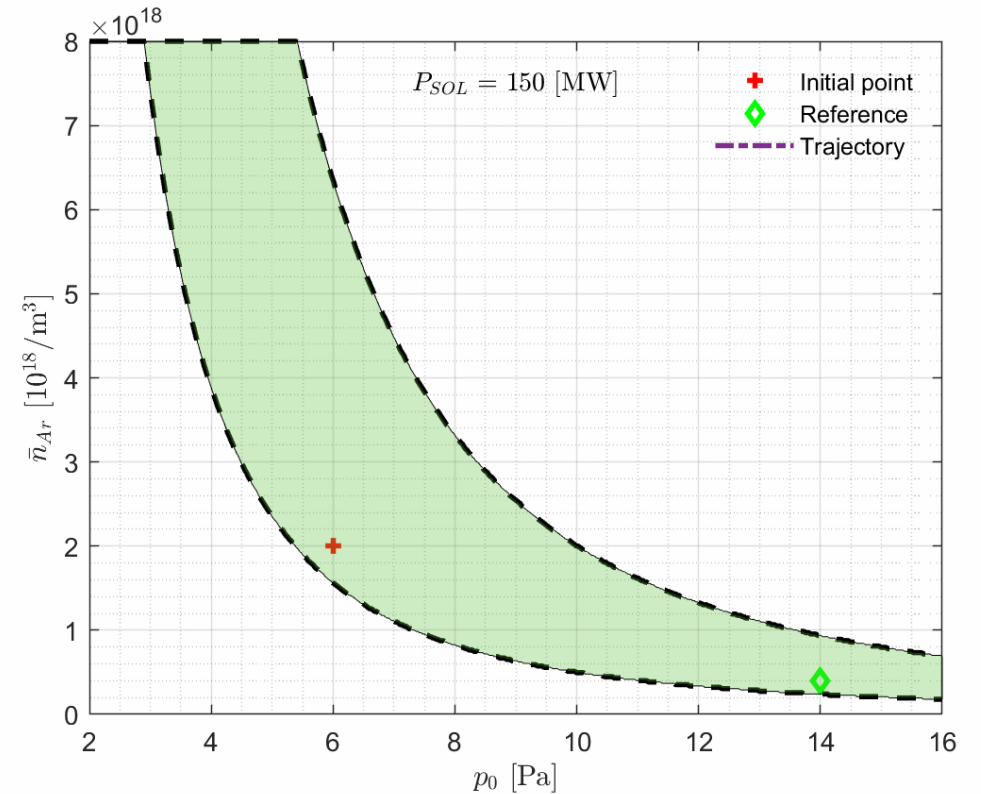


constrained map (simplified)

# Framework: ITPA DivSOL 2023 / Mosaic workshop 2023 (cont'd)



constrained map (simplified)

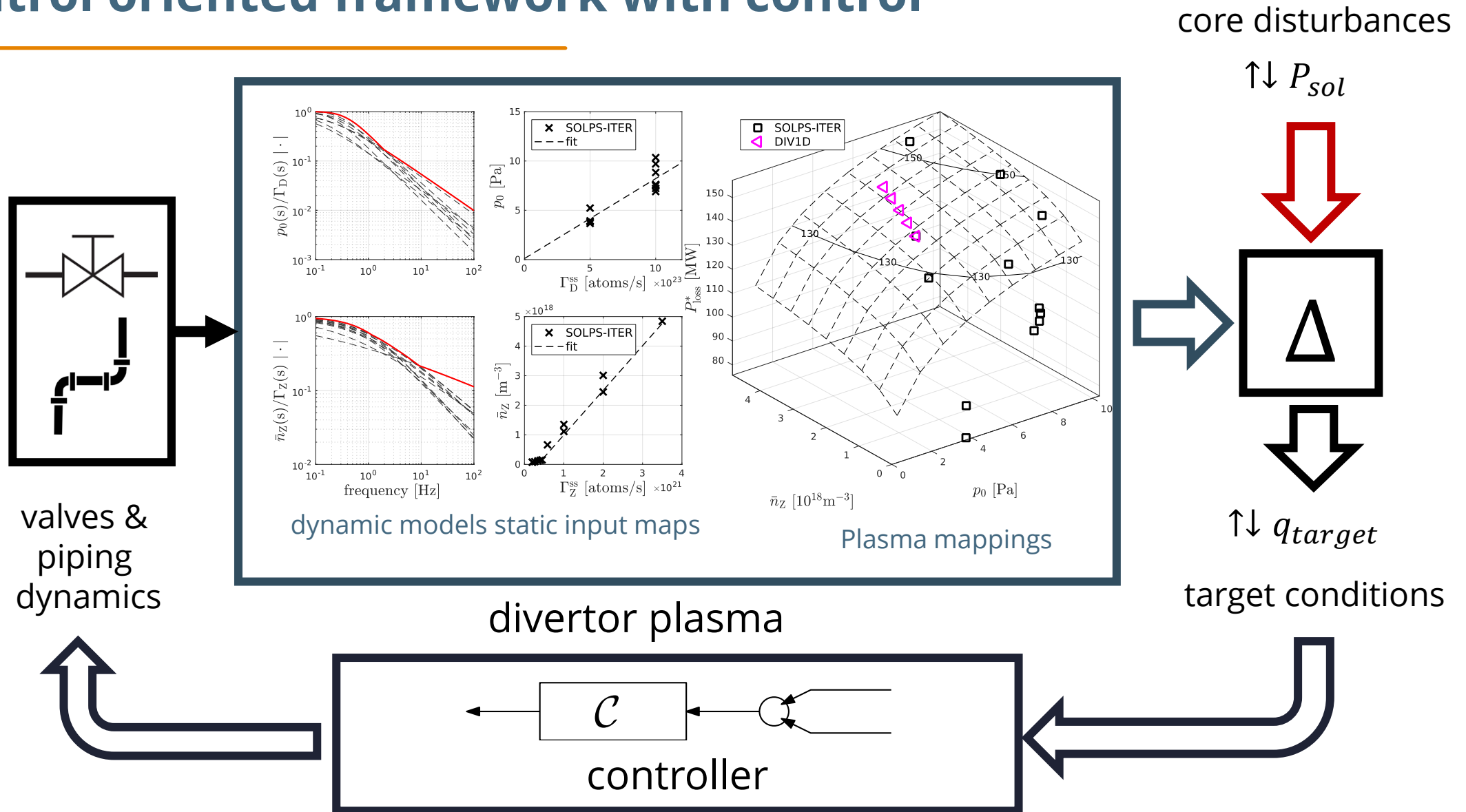


model predictive control (simplified)  
(dynamics included)



**Re-attachment times**

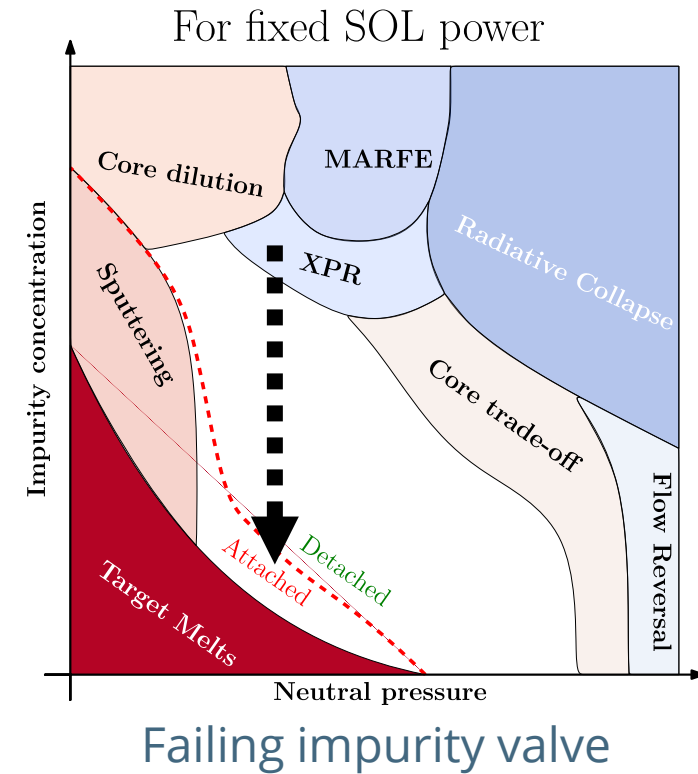
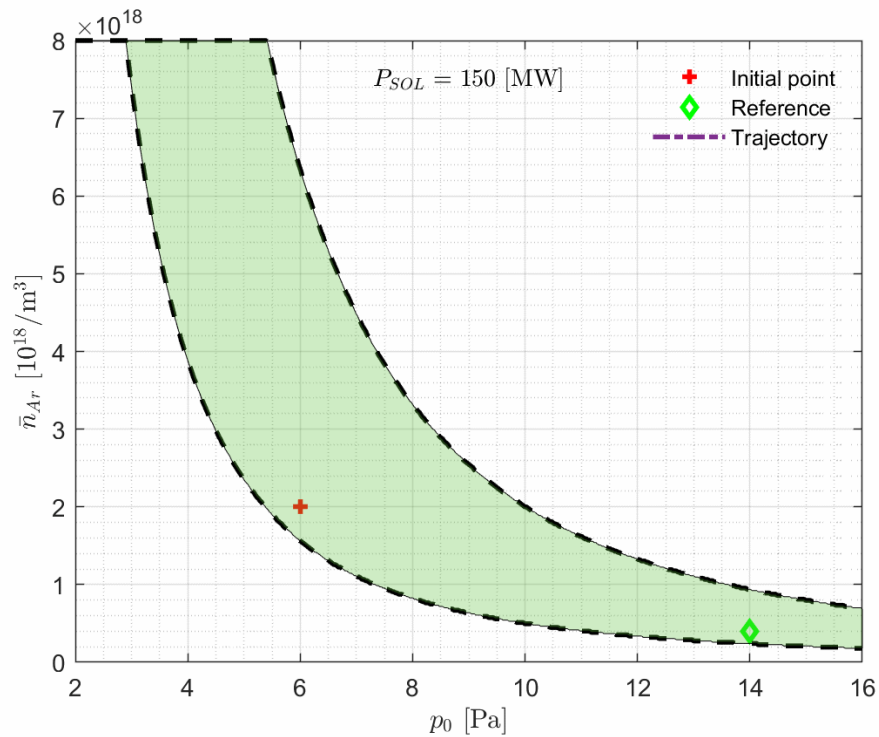
# Control oriented framework with control





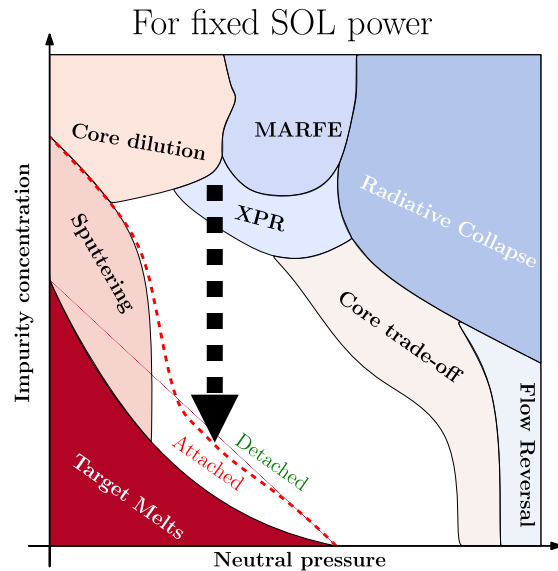
# Case study: time to re-attachment

- Re-attachment time-scale do not exist but there is a time to re-attachment:

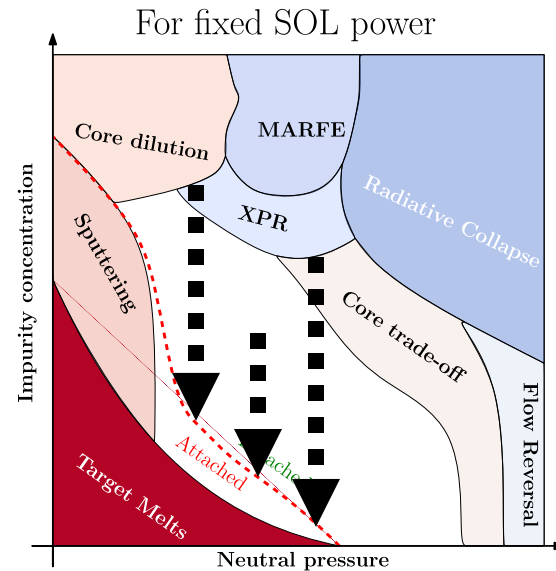


# Case study: time to re-attachment

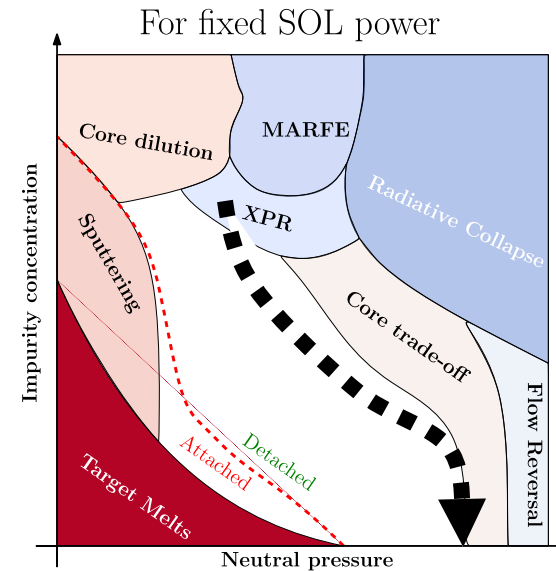
- Re-attachment time-scale do not exist but there is a time to re-attachment:



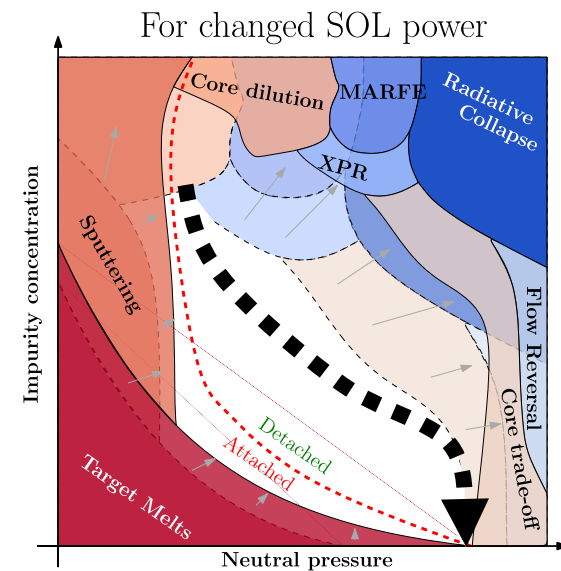
Failing impurity valve



Failing impurity valve  
(different initial conditions)

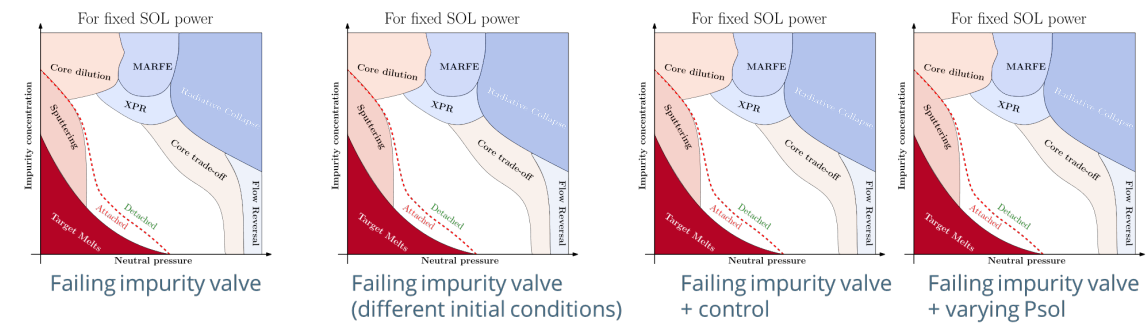


Failing impurity valve  
+ control



Failing impurity valve  
+ varying (increased)  
 $P_{sol}$

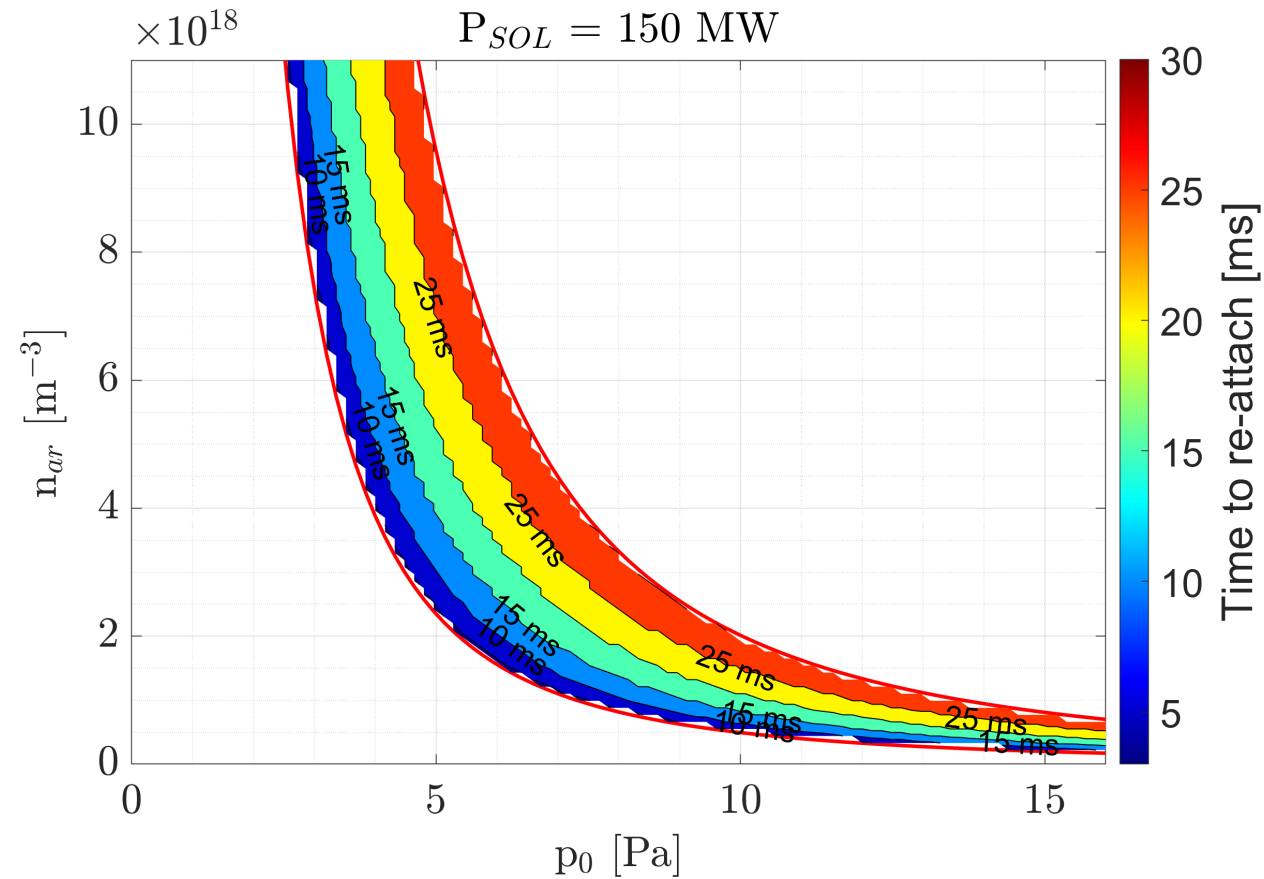
# Time to re-attachment



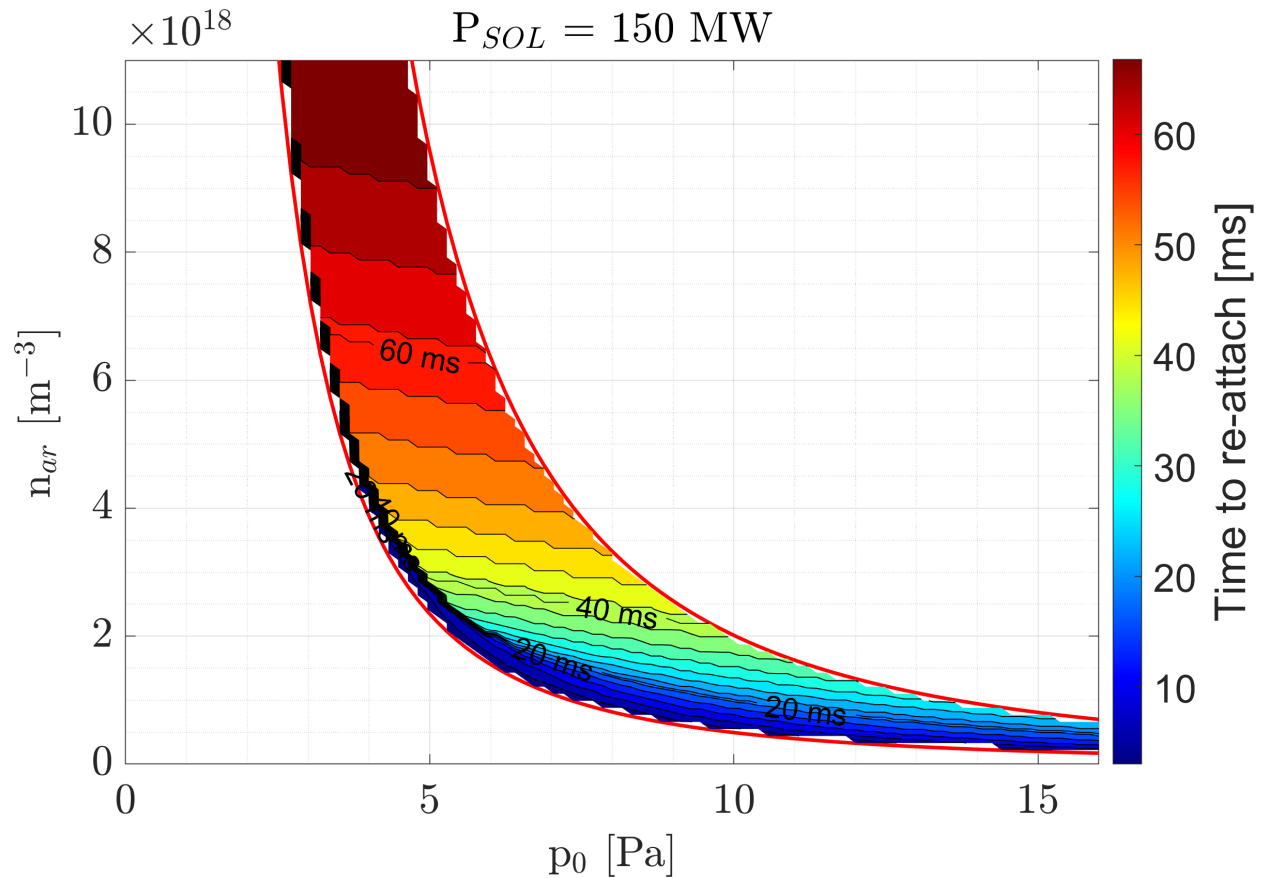
- Re-attachment time-scale does not exist but there is a time to re-attachment which depends on various factors:
  - plasma dynamics which is generally not one time-scale (but mixed time-scales), e.g., transport
    - an approximation of a time-constant exists but it is generally incomplete, especially for advanced control
  - valve + pipe have dynamics and can be well modelled by time-scales (first order system)
    - dominates generally the time-scale to re-attachment because its phase “delay”  $\gg$  phase “delay” of the plasma
  - initial condition (from where are we coming) and type of disturbance is critical to determine time to re-attachment
  - (model-predictive) control is there to counter-act re-attachment and increases the time to re-attachment significantly (if done correctly)

Hence, a complete model of all these components (digital twin) necessary to assess re-attachment times and scenarios

# What control can do when the impurity valve fails?



Without control

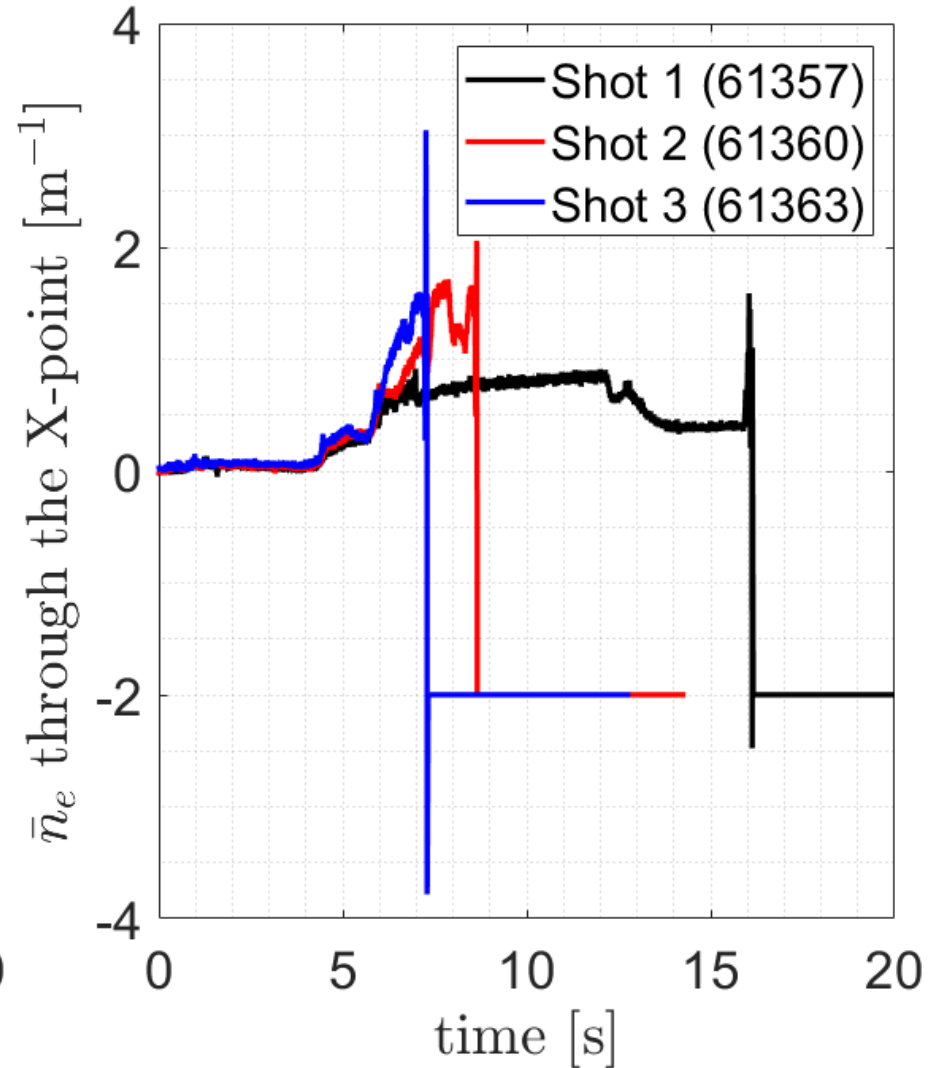
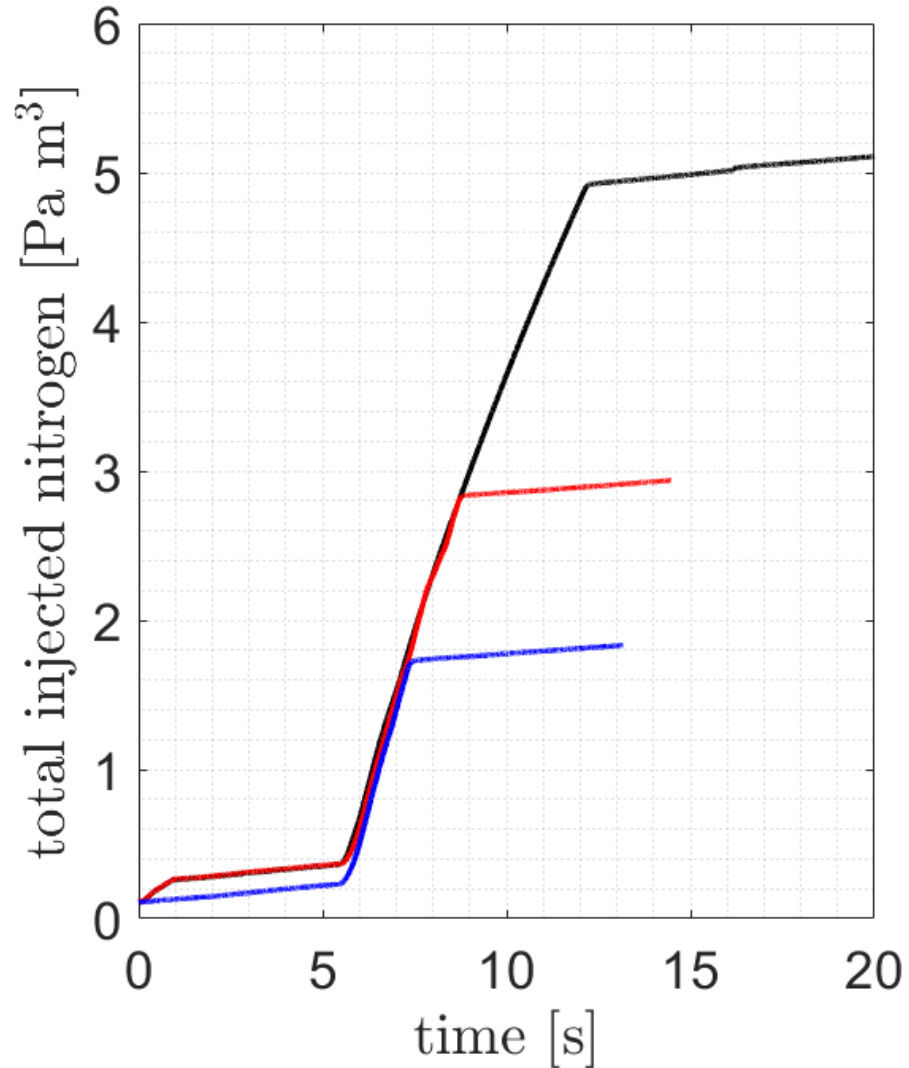


With MPC control



**Impurities vary from  
discharge to discharge**

# Challenge of highly radiative regimes: discharge history critical

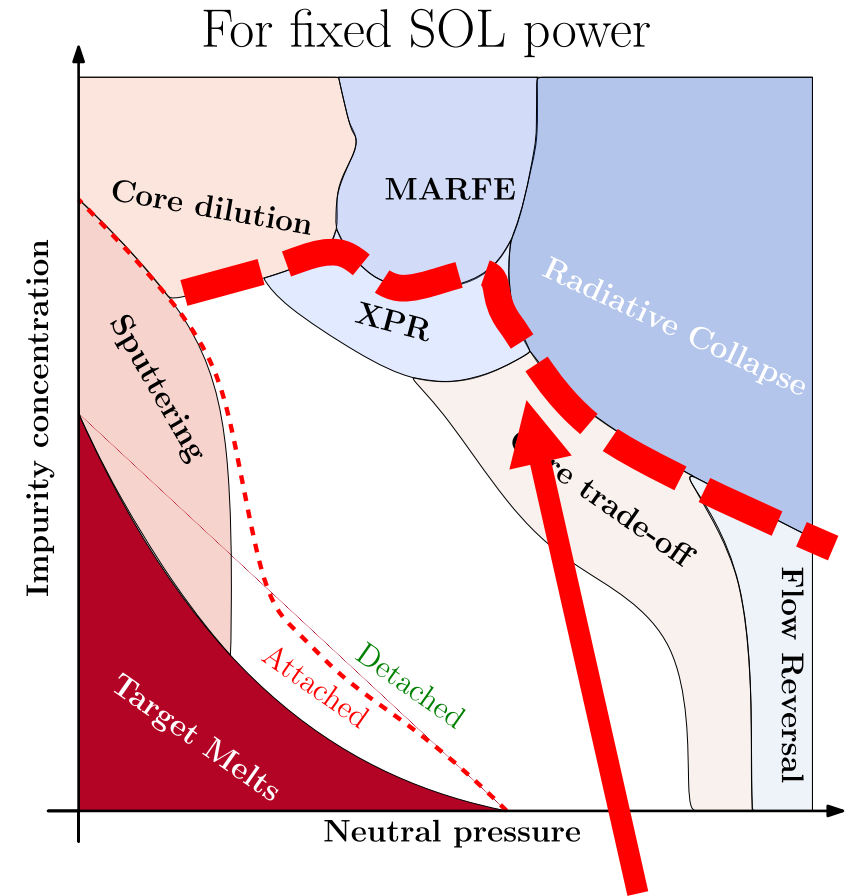




# Steps necessary to consistently develop highly radiative regimes

- Scenario development is predominantly a trial & error method
  - Due to varying initial concentrations of impurities, this method leads to continuous disruptions (overseeding)
  - Bad flow control (calibrations) or its absence contributes further
- Absolute observers are necessary and to be integrated in scenario development such that the levels can be observed correctly and controlled to quantitative values
- Consequently, scenario development is done on the correct levels of impurities, also can be embedded in which requested impurity levels are requested instead of “tried”

I believe this might reduce 100(s) of discharges per campaign over the machines



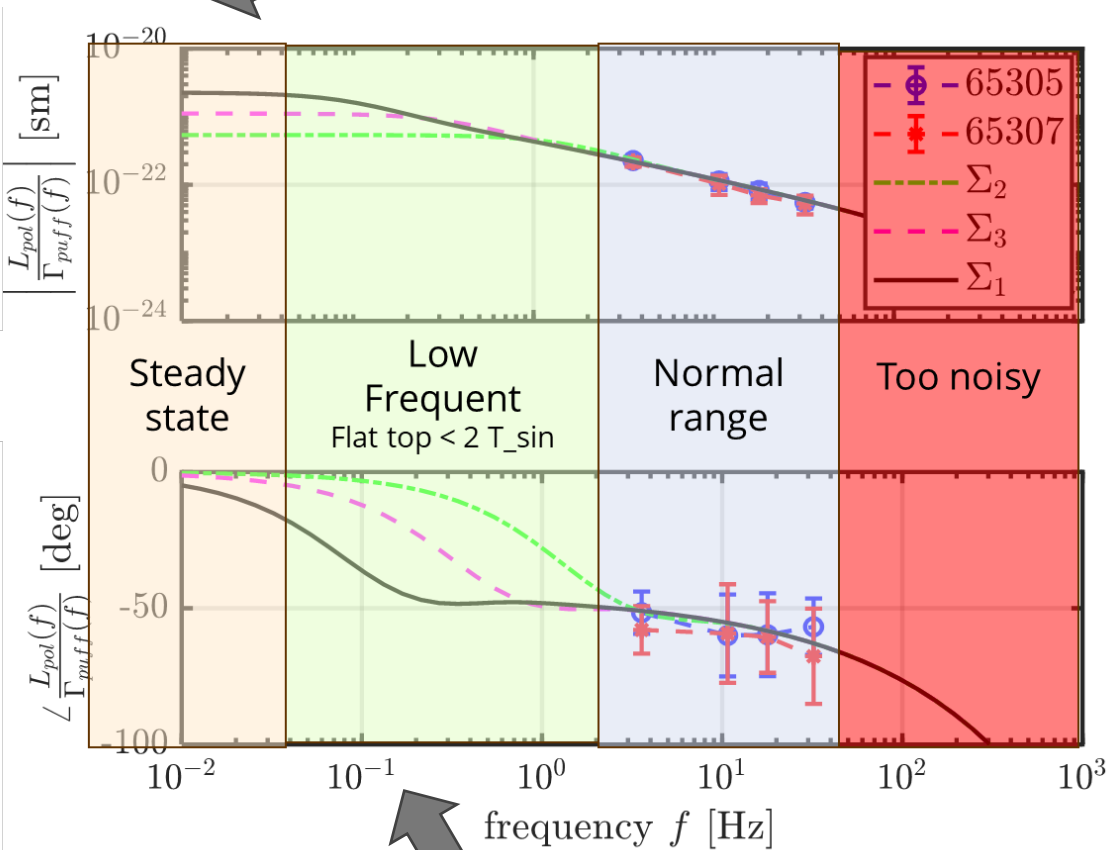
Assess (real) radiative limit  
not relative to injection



**What needs to be done?**

# Steps necessary for “digital twin”

Evaluate if quasi steady-state is valid



Find first dynamic transition(s) so-called poles

Complete dynamic relationship between actuators, disturbances and processes (frequency response functions over OP)

	Modulations for the exhaust						
Machines	DT	DD	N <sub>2</sub>	Ar	Ne	ECH	NBI
JET	✓	✓	✓	✓	✓	✗	✓
AUG	✗		✓	✓	✗	?	?
TCV	✗	✓	✓	✗	✗	✓	✓
DIII-D	✗	✓	✓	✗	✗	?	?
MAST-U	✗	✓	✗	✗	✗	✗	✗
WEST	✗	✗	✗	✗	✗	✗	✗

Table 1. ✓ one operating point, ✓ multiple operating points, ✗ not available

Extrapolation and interpolation for control “digital twin”

# Questions

What kind of fault scenarios do we expect to lead to reattachment?

- actuator failures
- observer failures
- disturbances (increasing the power, reduce radiation/momentum losses)

I am more worried to overseed in highly radiative regimes

What is a realistic assumption for the conditions at reattachement (Stuart spoke mostly about the timescales, but do we expect the heat to come down at  $\lambda_{\text{Eich}}$  or the QCE width, or somewhere in between)?

- this can be analyzed using variational analysis

Are there emergency actions other than sweeping that we could think off (like firing an impurity doped pellet into the divertor plasma)?

- (doped) pellets
- shorter gas-line
- more pumping capacity (over dimensioning the system)

# Core disturbances: dynamic error budgeting

$$PSD_x(f) = 2 \lim_{T \rightarrow \infty} \frac{1}{T} |\hat{x}(f)|^2,$$

## Motivation:

During operation, different disturbances will act on the divertor. Understanding their impact is crucial for control.

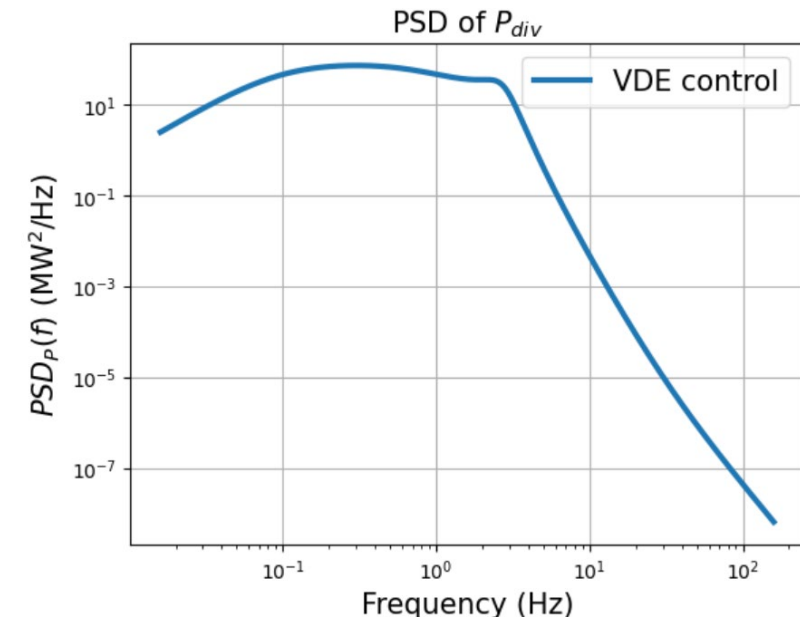
## Core disturbances (example STEP tokamak):

Continuous	Discrete
<ul style="list-style-type: none"><li>- Fusion Power Fluctuations</li><li>- RWM control</li><li>- VDE control</li></ul>	<ul style="list-style-type: none"><li>- Unexpected H-L transitions</li><li>- ECCH mode control</li><li>- (Large) Pellets</li><li>- W-flakes</li></ul>



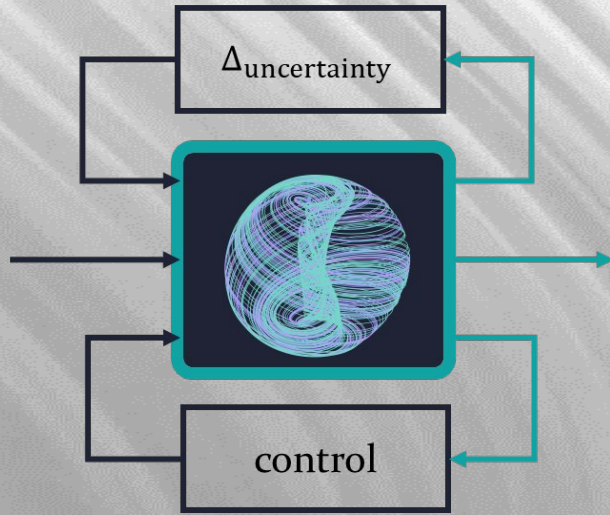
## Procedure:

- Characterize input disturbances in terms of  $PSD$ .



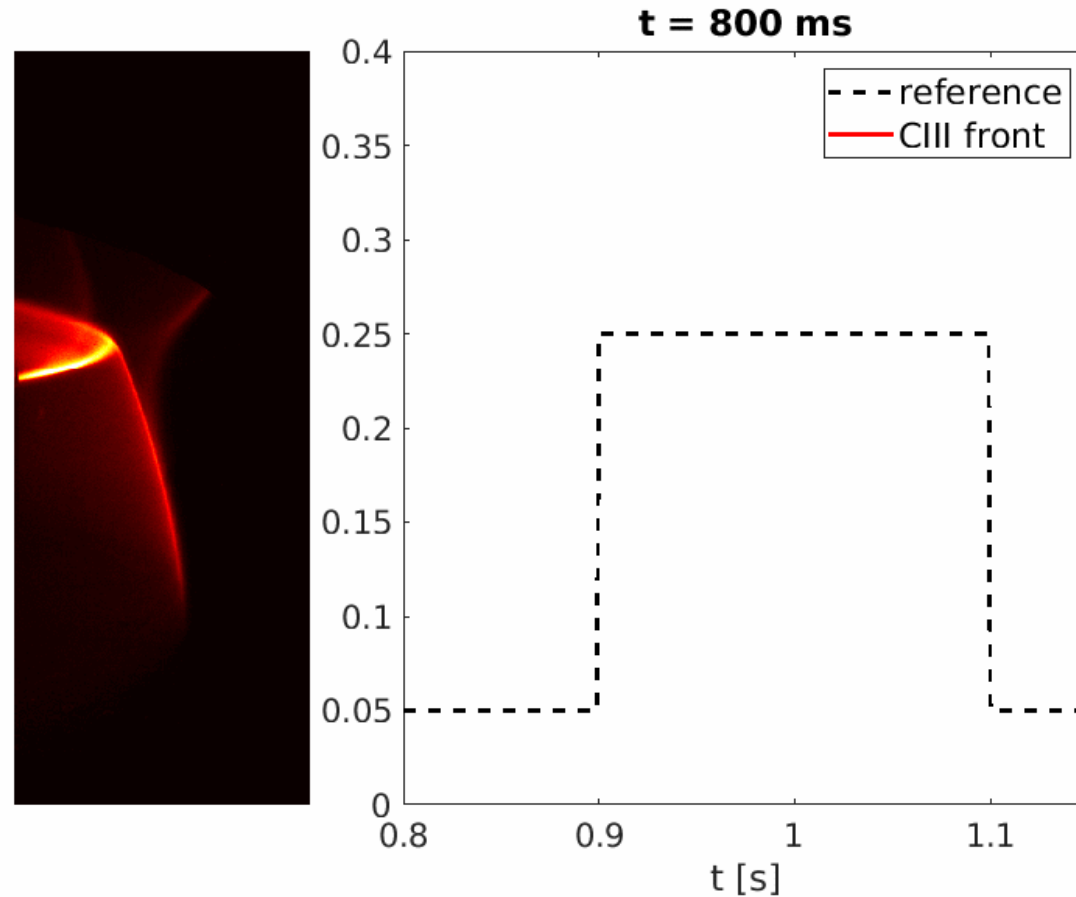


# ENERGY SYSTEMS & CONTROL





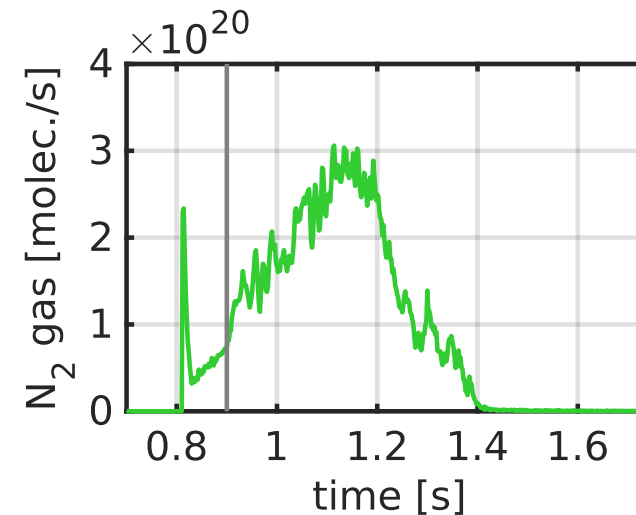
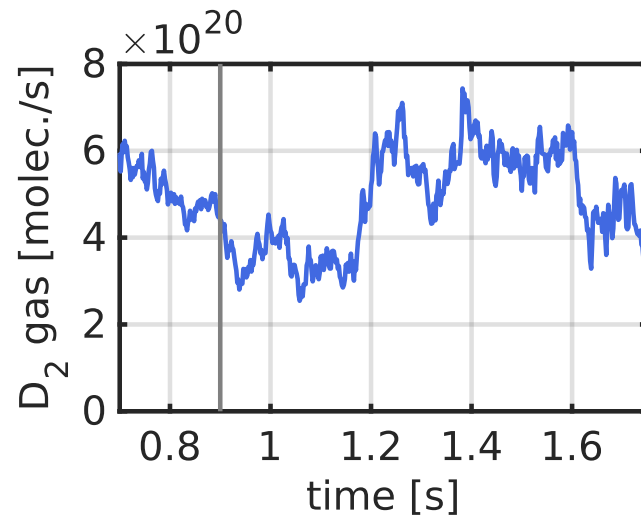
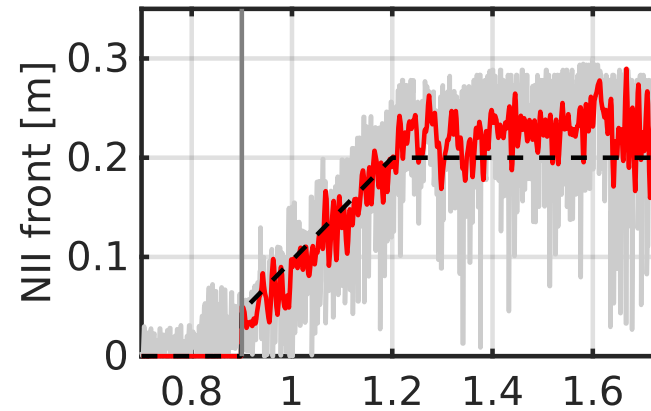
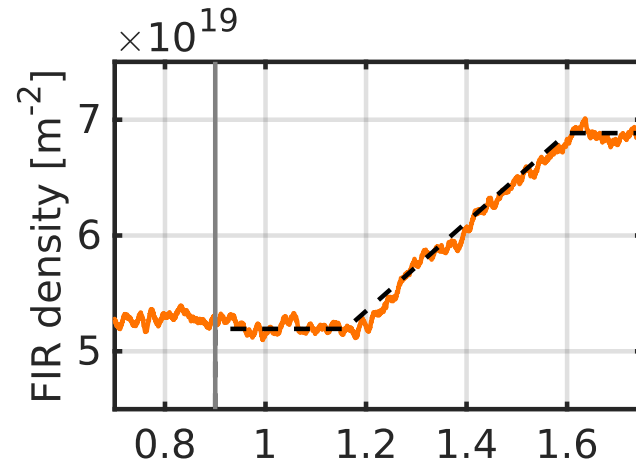
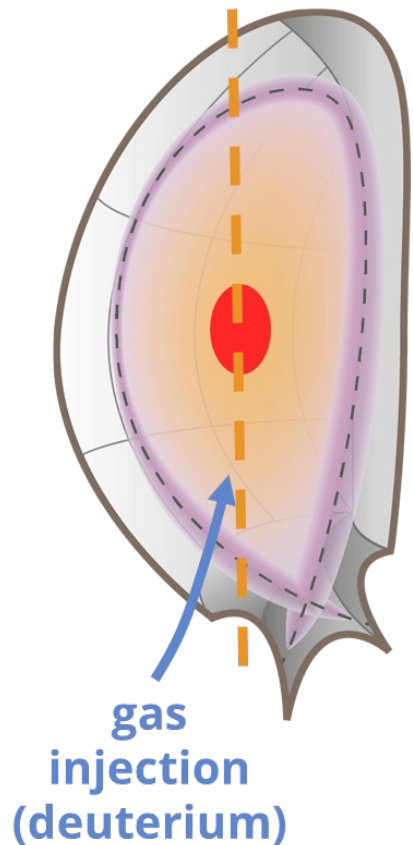
# Why it is important to know limits of the operational space?



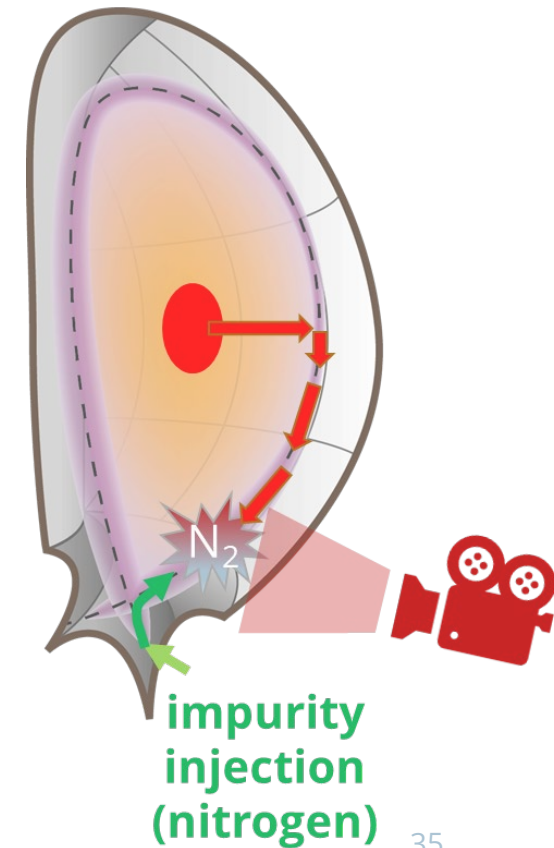
Build a model to describe all these aspects and avoid  
(unobserved states leading) to machine failure

# Joint core and exhaust control (multiple-input multiple-output)

interferometry



MANTIS camera

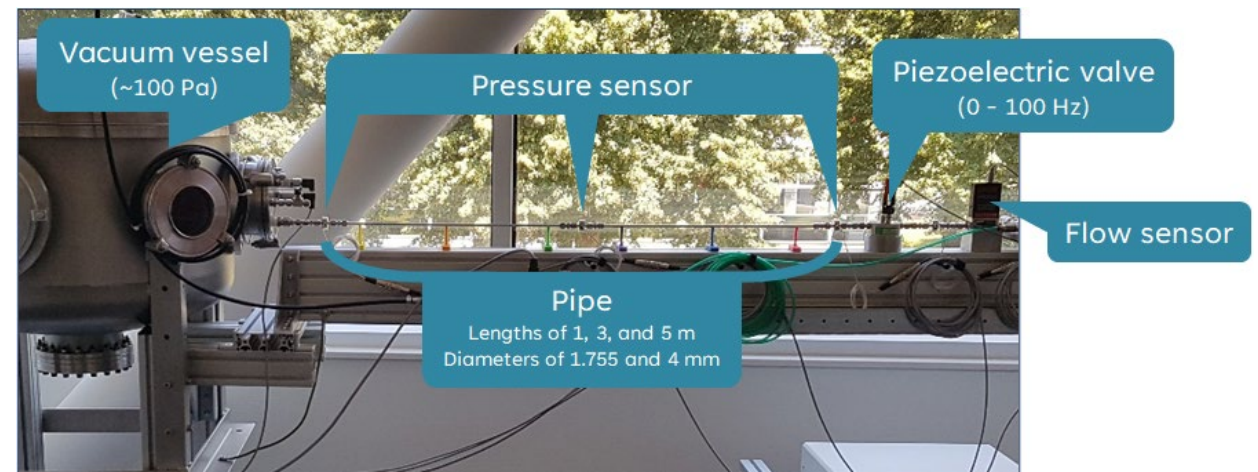


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# Piping dynamics

**Test, validate, and develop (data-driven) dynamic models on experimental gas setup**

- Pipe length introduces delayed response and **amplitude attenuation** between requested and actual gas injection.
- Validated low & high fidelity model
  - Long delays limit the ability to suppress fast transients



Gas flow test setup at DIFFER

